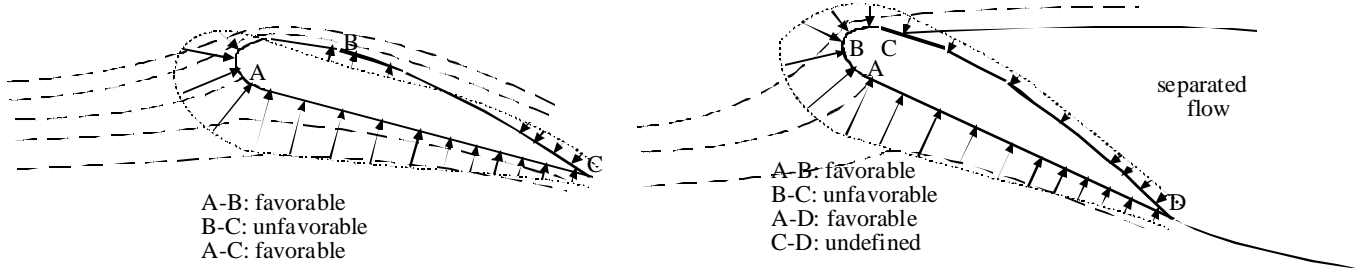


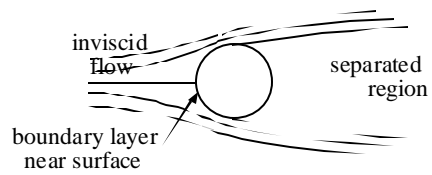
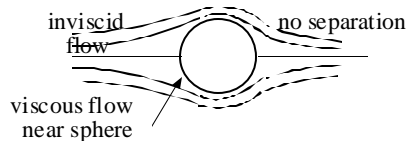
CHAPTER 8

External Flows

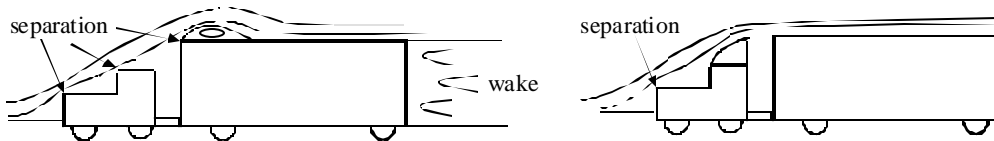
8.1



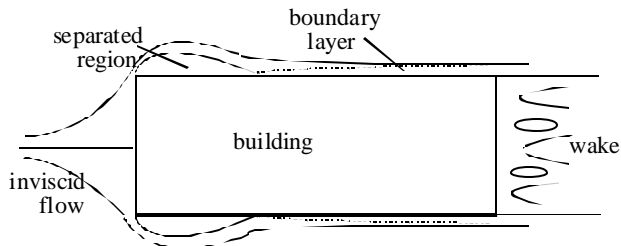
8.2 $Re = 5 = \frac{VD}{\nu} \therefore D = \frac{5 \times 1.51 \times 10^{-5}}{20} = 3.78 \times 10^{-5} \text{ m.}$



8.3



8.4



8.5 (C)

8.6 (C)

$$8.7 \quad (\mathbf{B}) \quad \text{Re} = \frac{VD}{\mathbf{n}} = \frac{0.8 \times 0.008}{1.31 \times 10^{-6}} = 4880.$$

$$8.8 \quad 5 = \frac{VD}{\mathbf{n}} \quad \therefore V = 5\mathbf{n} / D. \quad \text{a) } V = 5 \times 1.22 \times 10^{-5} / \frac{.8}{12} = \underline{.000915 \text{ fps.}}$$

$$\text{b) } V = 5 \times .388 \times 10^{-5} / \frac{.8}{12} = \underline{.000291 \text{ fps.}} \quad \text{c) } V = 5 \times 1.6 \times 10^{-4} / \frac{.8}{12} = \underline{0.012 \text{ fps.}}$$

$$8.9 \quad \text{Re} = \frac{VD}{\mathbf{n}} = \frac{20 \times D}{1.51 \times 10^{-5}} = 13.25 \times 10^5 D.$$

$$\text{a) } \text{Re} = 13.25 \times 10^5 \times 6 = \underline{7.9 \times 10^6}. \quad \therefore \text{Separated flow.}$$

$$\text{b) } \text{Re} = 13.25 \times 10^5 \times .06 = \underline{7.9 \times 10^4}. \quad \therefore \text{Separated flow.}$$

$$\text{c) } \text{Re} = 13.25 \times 10^5 \times .006 = \underline{7950}. \quad \therefore \text{Separated flow.}$$

$$8.10 \quad F_D = \int_{A_{\text{front}}} p dA - p_{\text{back}} A_{\text{back}} = p_0 \int_0^1 (1 - r^2) 2pr dr = p_0 2p \left(\frac{1}{2} - \frac{1}{4} \right) = \frac{1}{2} p p_0$$

$$\text{Bernoulli: } p_{\infty} + \frac{1}{2} r V_{\infty}^2 = p_0. \quad \therefore p_0 = \frac{1}{2} \times 1.21 \times 20^2 = 242 \text{ Pa.}$$

$$\therefore F_D = \frac{1}{2} p (242) = \underline{380 \text{ N}}$$

$$C_D = \frac{F_D}{\frac{1}{2} r V^2 A} = \frac{2 \times 380}{1.21 \times 20^2 \times p \times 1^2} = \underline{0.5}$$

$$8.11 \quad F_{\text{total}} = F_{\text{bottom}} + F_{\text{top}} = 20\,000 \times .3 \times .3 + 10\,000 \times .3 \times .3 = 2700 \text{ N.}$$

$$F_{\text{lift}} = 2700 \cos 10^\circ = \underline{2659 \text{ N}}$$

$$F_{\text{drag}} = 2700 \sin 10^\circ = \underline{469 \text{ N}}$$

$$C_L = \frac{F_L}{\frac{1}{2} r V^2 A} = \frac{2 \times 2659}{1000 \times 5^2 \times .3 \times .3} = \underline{2.36}$$

$$C_D = \frac{F_D}{\frac{1}{2} r V^2 A} = \frac{2 \times 469}{1000 \times 5^2 \times .3 \times .3} = \underline{0.417}$$

$$8.12 \quad F_{\ell} = p_{\ell} A_{\ell} = 26\,000 \times Lw. \quad F_u = p_u A_u = 8000 \times \frac{Lw}{2 \cos 5^\circ} = 4015 Lw$$

$$F_L = F_{\ell} \cos 5^\circ - F_u \cos 10^\circ = 21\,950 Lw$$

$$F_D = F_{\ell} \sin 5^\circ - F_u \sin 10^\circ = 1569 Lw$$

$$C_L = \frac{F_L}{\frac{1}{2} \rho V^2 A} = \frac{2 \times 21\,950 LW}{.3119 \times 750^2 LW} = \underline{0.25}$$

$$C_D = \frac{F_D}{\frac{1}{2} \rho V^2 A} = \frac{2 \times 1569 LW}{.3119 \times 750^2 LW} = \underline{0.0179}$$

8.13 If $C_D = 1.0$ for a sphere, $Re = 100$ (see Fig. 8.8). $\therefore \frac{V \times .1}{n} = 100, V = 1000n.$

a) $V = 1000 \times 1.46 \times 10^{-5} = .0146 \text{ m/s}. \therefore F_D = \frac{1}{2} \times 1.22 \times .0146^2 \rho \times .05^2 \times 1.0$
 $= \underline{3.25 \times 10^{-7} \text{ N.}}$

b) $V = 1000 \times \frac{1.46 \times 10^{-5}}{.015 \times 1.22} = 0.798 \text{ m/s}. \therefore F_D = \frac{1}{2} \times (.015 \times 1.22) \times .798^2 \rho \times .05^2 \times 1.0$
 $= \underline{4.58 \times 10^{-5} \text{ N.}}$

c) $V = 1000 \times 1.31 \times 10^{-6} = .00131 \text{ m/s}. \therefore F_D = \frac{1}{2} \times 1000 \times .00131^2 \rho \times .05^2 \times 1.0$
 $= \underline{6.74 \times 10^{-6} \text{ N.}}$

8.14 a) $Re = \frac{VD}{n} = \frac{6 \times .5}{1.5 \times 10^{-5}} = 2 \times 10^5. \therefore C_D = 0.45$ from Fig. 8.8.

$$\therefore F_D = \frac{1}{2} \rho V^2 A C_D = \frac{1}{2} \times 1.22 \times 6^2 \times \rho \times .25^2 \times .45 = 1.94 \text{ N.}$$

b) $Re = \frac{15 \times .5}{1.5 \times 10^{-5}} = 5 \times 10^5. \therefore C_D = 0.2$ from Fig. 8.8.

$$\therefore F_D = \frac{1}{2} \rho V^2 A C_D = \frac{1}{2} \times 1.22 \times 15^2 \times \rho \times .25^2 \times .2 = 5.4 \text{ N.}$$

8.15 (B) Assume a large Reynolds number so that $C_D = 0.2$. Then

$$F = \frac{1}{2} \rho V^2 A C_D = \frac{1}{2} \times 1.23 \times \left(\frac{80 \times 1000}{3600} \right)^2 \times \rho \times 5^2 \times 0.2 = 4770 \text{ N.}$$

8.16 (D) Assume a Reynolds number of 10^5 . Then $C_D = 1.2$.

$$F = \frac{1}{2} \rho V^2 A C_D. \therefore 60 = \frac{1}{2} \times 1.23 \times 40^2 \times 4 \times D \times 1.2. \therefore D = 0.0041 \text{ m.}$$

$$Re = \frac{VD}{n} = \frac{40 \times 0.0041}{10^{-6}} = 1.64 \times 10^5. \therefore C_D = 1.2. \text{ The assumption was OK.}$$

8.17 The velocities associated with the two Re's are

$$V_1 = \frac{\text{Re}_1 n}{D} = \frac{3 \times 10^5 \times 1.5 \times 10^{-5}}{.0445} = 101 \text{ m/s},$$

$$V_2 = \frac{\text{Re}_2 n}{D} = \frac{6 \times 10^4 \times 1.5 \times 10^{-5}}{.0445} = 20 \text{ m/s}.$$

The drag, between these two velocities, is reduced by a factor of 2.5

$\left[(C_D)_{\text{high}} = 0.5 \text{ and } (C_D)_{\text{low}} = 0.2 \right]$. Thus, between 20 m/s and 100 m/s the drag is reduced by a factor of 2.5. This would significantly lengthen the flight of the ball.

8.18 a) $F_D = \frac{1}{2} \rho V^2 A C_D. \quad \therefore 0.5 = \frac{1}{2} \times .00238 V^2 \rho \times \left(\frac{2}{12} \right)^2 C_D. \quad \therefore V^2 C_D = 4810.$

$$\text{Re} = \frac{VD}{n} = \frac{V \times 4 / 12}{1.6 \times 10^{-4}} = 2080V. \quad \text{Try } C_D = .5: \quad V = 98 \text{ fps, Re} = 2 \times 10^5.$$

$$\text{Try } C_D = .4: \quad V = \underline{110 \text{ fps}}, \text{ Re} = 2.3 \times 10^5.$$

b) $C_D = 0.2: \quad 0.5 = \frac{1}{2} \times .00238 V^2 \rho \times \left(\frac{2}{12} \right)^2 \times 2. \quad \therefore V = \underline{155 \text{ fps}}.$

8.19 $4.2 = \frac{1}{2} \times 1000 V^2 \rho \times .1^2 C_D. \quad \therefore V^2 C_D = 0.267. \quad \text{Re} = \frac{V \times .2}{10^{-6}} = 2 \times 10^5 V.$

Try $C_D = 0.5: \quad \therefore V = 0.73 \text{ m/s. Re} = \underline{1.46 \times 10^5}. \quad \therefore \text{OK}.$

8.20 $\text{Re} = \frac{VD}{n} = \frac{40 \times 2}{1.5 \times 10^{-5}} = 5.3 \times 10^6. \quad \therefore C_D = 0.7. \quad (\text{This is extrapolated from$

Fig. 8.8.) $\therefore F_D = \frac{1}{2} \times 1.22 \times 40^2 \times (2 \times 60) \times .7 = \underline{81\,900 \text{ N}}.$

$$M = 81\,900 \times 30 = \underline{2.46 \times 10^6 \text{ N}\cdot\text{m}}.$$

8.21 a) $\text{Re}_1 = \frac{25 \times .05}{1.08 \times 10^{-5}} = 1.2 \times 10^5. \quad \text{Re}_2 = 1.8 \times 10^5. \quad \text{Re}_3 = 2.4 \times 10^5. \quad \text{Assume a rough cylinder (the air is highly turbulent).}$

$$\therefore (C_D)_1 = 0.7, (C_D)_2 = 0.8, (C_D)_3 = 0.9.$$

$$\therefore F_D = \frac{1}{2} \times 1.45 \times 25^2 (.05 \times 10 \times .7 + .075 \times 15 \times .8 + .1 \times 20 \times .9) = \underline{1380 \text{ N}}.$$

$$M = \frac{1}{2} \times 1.45 \times 25^2 (.05 \times 10 \times .7 \times 40 + .075 \times 15 \times .8 \times 27.5 + .1 \times 20 \times .9 \times 10) = \underline{25\,700 \text{ N}\cdot\text{m}}.$$

b) $\text{Re}_1 = \frac{25 \times .05}{1.65 \times 10^{-5}} = 7.6 \times 10^4. \quad \text{Re}_2 = 1.14 \times 10^5, \quad \text{Re}_3 = 1.5 \times 10^5.$

$$\therefore (C_D)_1 = 8, (C_D)_2 = 7, (C_D)_3 = 8. \quad r = \frac{101}{.287 \times 308} = 1.17 \text{ kg/m}^3.$$

$$\therefore F_D = \frac{1}{2} \times 1.17 \times 25^2 (.05 \times 10 \times 8 + .075 \times 15 \times 7 + 1 \times 20 \times 8) = \underline{1020 \text{ N}}.$$

$$M = \frac{1}{2} \times 1.17 \times 25^2 (.05 \times 10 \times 8 \times 40 + .075 \times 15 \times 7 \times 27.5 + 1 \times 20 \times 8 \times 10) = \underline{19\,600 \text{ N} \cdot \text{m}}.$$

8.22 Atmospheric air is turbulent. \therefore Use the "rough" curve. $\therefore C_D = 0.7$.

$$F_D = 10 = \frac{1}{2} \times .00238 V^2 \times 6 D \times 7. \quad \therefore 2000 = V^2 D. \quad 10^5 = \frac{V \times 2000 / V^2}{1.6 \times 10^{-4}}.$$

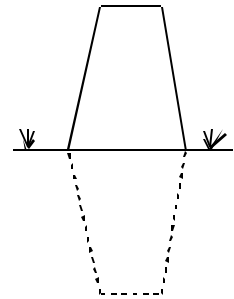
$$\therefore p_{\min} = \frac{\rho}{2} [U_\infty^2 - v_o^2] = \frac{0.0024}{2} [30^2 - 104^2] = \underline{-11.8 \text{ psf}}.$$

$$\therefore V^2 D = 2370. \quad \therefore V = \underline{148 \text{ fps}}. \quad D = \underline{0.108'}.$$

8.23 Since the air cannot flow around the bottom, we imagine the structure to be mirrored as shown. Then $L/D = 40/5 = 8$. $\therefore C_D = 0.66 C_{D_{\infty}}$.

$$\text{Re}_{\min} = \frac{VD_{\min}}{\nu} = \frac{30 \times 2}{1.5 \times 10^{-5}} = 4 \times 10^6. \quad \therefore C_D = 1.0 \times .66 = .66.$$

$$\therefore F_D = \frac{1}{2} \times 1.22 \times 30^2 \times \left(\frac{2+8}{2} \times 20 \right) \times .66 = \underline{36\,000 \text{ N}}.$$

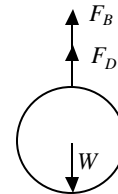


8.24

$$F_B + F_D = F_W.$$

$$9810 \times \frac{4}{3} \rho r^3 + \frac{1}{2} \times 1000 V^2 \rho r^2 C_D = 9810 \times 7.82 \times \frac{4}{3} \rho r^3.$$

$$\text{Re} = \frac{V \times 2r}{10^{-6}} = 2 \times 10^6 V r. \quad \therefore V^2 C_D = 178 r$$



a) $r = .05 \text{ m}$. $\therefore \text{Re} = 10^5 V$, $V^2 C_D = 8.9$. Assume a smooth sphere.

Try $C_D = 5$: $\therefore V = 4.22 \text{ m/s}$. $\text{Re} = 4.22 \times 10^5$. This is too large for Re .

Try $C_D = 2$: $\therefore V = \underline{6.67 \text{ m/s}}$. $\text{Re} = 6.67 \times 10^5$. OK.

b) $r = .025 \text{ m}$. $\text{Re} = 5 \times 10^4 V$, $V^2 C_D = 4.45$.

Try $C_D = 2$: $V = \underline{4.72 \text{ m/s}}$. $\text{Re} = 2.4 \times 10^5$. OK.

c) $r = .005 \text{ m}$. $\text{Re} = 10^4 V$, $V^2 C_D = 0.89$.

Try $C_D = 5$: $V = \underline{1.33 \text{ m/s}}$. $\text{Re} = 1.33 \times 10^4$. OK.

d) $r = .001 \text{ m}$. $\text{Re} = 2 \times 10^3 V$, $V^2 C_D = 0.178$.

Try $C_D = 4$: $V = \underline{0.67 \text{ m/s}}$. $\text{Re} = 1.33 \times 10^3$. OK.

$$8.25 \quad F_B + F_D = F_W. \quad .077 \times \frac{4}{3} \rho \left(\frac{10}{12} \right)^3 + \frac{1}{2} \times .00238 V^2 \rho \left(\frac{10}{12} \right)^2 C_D = 62.4 S \frac{4}{3} \rho \left(\frac{10}{12} \right)^3.$$

$$\text{Re} = \frac{V \times 10/12}{1.6 \times 10^{-4}} = 5.2 \times 10^3 V. \quad \therefore 1 + .0139 V^2 C_D = 810 S$$

a) $S = .005$. $V^2 C_D = 219$. Assume atmospheric turbulence, i.e., rough.

Try $C_D = .4$: $V = 23.4$ fps. $\text{Re} = 1.2 \times 10^5$. $\therefore C_D = .3$. $V = \underline{27}$ fps.

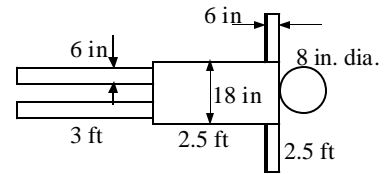
b) $S = .02$. $V^2 C_D = 1090$. Try $C_D = .4$: $V = \underline{52}$ fps. $\text{Re} = 2.7 \times 10^5$. \therefore OK.

c) $S = 1.0$. $V^2 C_D = 58\,200$. Try $C_D = .4$: $V = \underline{381}$ fps.

8.26

Assume a 180 lb, 6' sky diver, with components as shown. If V is quite large, then $\text{Re} > 2 \times 10^5$.

$$F_D = F_W.$$



$$\frac{1}{2} \times .00238 V^2 \left[2 \times 3 \times \frac{1}{2} \times 1.0 \times .7 + 2 \times 2.5 \times \frac{1}{2} \times 1.0 \times .7 + \frac{18}{12} \times 2.5 \times 1.0 + \rho \times \left(\frac{4}{12} \right) \times .4 \right] = 180.$$

We used data from Table 8.1. $\therefore V = \underline{140}$ fps.

$$8.27 \quad \text{From Table 8.2 } C_D = 0.35. \quad F_D = \frac{1}{2} \times 1.22 V^2 \times 3.2 \times 0.35 = .683 V^2.$$

$$\text{a) } F_D = .683 \times \left(\frac{80 \times 1000}{3600} \right)^2 = 337 \text{ N. } \therefore \dot{W} = 337 \frac{80 \times 1000}{3600} = 7500 \text{ W or } \underline{10 \text{ Hp.}}$$

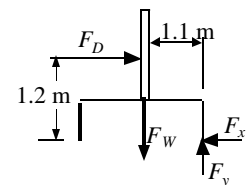
$$\text{b) } V = 25 \text{ m/s. } F_D = .683 \times 25^2 = 427 \text{ N. } \therefore \dot{W} = 427 \times 25 = 10\,700 \text{ W or } \underline{14.3 \text{ Hp.}}$$

$$\text{c) } V = 27.8 \text{ m/s. } F_D = .683 \times 27.8^2 = 527 \text{ N. } \therefore \dot{W} = 527 \times 27.8 = 14\,700 \text{ W or } \underline{19.6 \text{ Hp.}}$$

$$8.28 \quad 1.2 F_D = 1.1 \times 400. \quad F_D = \frac{1}{2} \rho V^2 A C_D. \quad C_D = 1.1$$

$$1.2 \times \frac{1}{2} \times 1.22 V^2 \times (2 \times 3) \times 1.1 = 1.1 \times 400.$$

$$\therefore V = \underline{9.5 \text{ m/s.}}$$



$$8.29 \quad \text{Re} = \frac{VD}{\nu} = \frac{(40\,000 / 3600) 0.6}{1.51 \times 10^{-5}} = 4.42 \times 10^5. \quad \therefore C_D = 0.35 \text{ from Fig. 8.8.}$$

$$\text{a) } F_D = \frac{1}{2} \rho V^2 A C_D = \frac{1}{2} \times 1.204 \times (40\,000 / 3600)^2 \times 0.6 \times 6 \times 0.35 = \underline{93.6 \text{ N}}$$

$$\text{b) } F_D = 93.6 \times 0.68 = \underline{63.7 \text{ N}} \text{ where } L/D = 6 / 0.6 = 10.$$

c) $F_D = 93.6 \times 0.76 = \underline{71.1 \text{ N}}$ where we can use $L/D = 20$ since only one end is free. The ground acts like the mid-section of a 12-m-long cylinder.

- 8.30 a) Curled up, she makes an approximate sphere of about 1.2 m in diameter (just a guess!). Assume a rough sphere at large Re. From Fig. 8.8, $C_D = 0.4$:

$$F_D = \frac{1}{2} \rho V^2 A C_D$$

$$80 \times 9.8 = \frac{1}{2} \times 1.21 \times V^2 \rho \times 0.6^2 \times 0.4. \quad \therefore V = \underline{53.7 \text{ m/s.}}$$

$$\text{Check Re: } Re = \frac{53.7 \times 1.2}{1.51 \times 10^{-5}} = 4.27 \times 10^6. \quad \therefore \text{OK.}$$

- b) $F_D = \frac{1}{2} \rho V^2 A C_D$. From Table 8.2, $C_D = 1.4$:

$$80 \times 9.8 = \frac{1}{2} \times 1.21 \times V^2 \rho \times 4^2 \times 1.4. \quad \therefore V = \underline{4.29 \text{ m/s.}}$$

$$\text{Check Re: } Re = \frac{4.29 \times 8}{1.51 \times 10^{-5}} = 2.27 \times 10^6. \quad \text{Should be larger but the velocity should be close.}$$

- c) $F_D = \frac{1}{2} \rho V^2 A C_D$

$$80 \times 9.8 = \frac{1}{2} \times 1.21 \times V^2 \rho \times 1^2 \times 1.4. \quad \therefore V = \underline{17.2 \text{ m/s.}}$$

$$\text{Check Re: } Re = \frac{17.2 \times 1}{1.51 \times 10^{-5}} = 1.14 \times 10^6. \quad \text{This should be greater than } 10^7 \text{ for } C_D \text{ to be acceptable. Hence, the velocity is approximate.}$$

- 8.31 With the deflector the drag coefficient is 0.76 rather than 0.96. The required power (directly related to fuel consumed) is reduced by the ratio of 0.76/0.96. The cost per year without the deflector is

$$\text{Cost} = (200\,000/1.2) \times 0.25 = \$41,667.$$

With the deflector it is

$$\text{Cost} = 41,667 \times 0.76/0.96 = \$32,986.$$

The savings is $\$41,667 - 32,986 = \$8,800$.

- 8.32 $F_D = \frac{1}{2} \rho V^2 A C_D = \frac{1}{2} \times .00238 \times 88^2 \times (6 \times 2) \times 1.1 = 122 \text{ lb.}$

$$\dot{W} = F_D \times V = 122 \times 88 = 10,700 \frac{\text{ft} \cdot \text{lb}}{\text{sec}} \quad \text{or} \quad \underline{19.5 \text{ Hp.}}$$

- 8.33 $F_D = \frac{1}{2} \rho V^2 A C_D = \frac{1}{2} \times 1.22 \times (27.8 \times 1.6)^2 \times \rho \times .05^2 \times 1.1 = 10.43 \text{ N.}$

$$\dot{W} = F_D \times V \times 2 = 10.43 \times (27.8 \times 1.6) \times 2 = 226 \text{ W} \quad \text{or} \quad \underline{1.24 \text{ Hp.}}$$

8.34 The projected area is $\frac{(2 + 0.3)}{2} \times 4 = 4.6 \text{ m}^2$.

$$F_D = \frac{1}{2} \rho V^2 A C_D = \frac{1}{2} \times 1.18 \times 20^2 \times 4.6 \times 0.4 = 434 \text{ N.}$$

Since there are two free ends, we use Table 8.1 with $L/D = 4 / 1.15 = 3.47$, and approximate the force as

$$F_D = 434 \times 0.62 = \underline{269 \text{ N.}}$$

8.35 The net force acting up is (use absolute pressure)

$$F_{\text{up}} = \frac{4}{3} \rho \times 0.4^3 \times 1.21 \times 9.8 - 0.5 \frac{4}{3} \rho \times 0.4^3 \frac{120}{2.077 \times 293} \times 9.8 = 2.16 \text{ N}$$

From a force triangle (2.16 N up and F_D to the right), we see that

$$\tan \alpha = F_{\text{up}} / F_D.$$

a) $F_D = 2.16 / \tan 80^\circ = 0.381$.

$$0.381 = \frac{1}{2} \times 1.21 V^2 \rho \times 0.4^2 \times 0.2. \quad \therefore V = 2.50 \text{ m/s.}$$

Check Re: $\text{Re} = \frac{2.5 \times 0.8}{1.51 \times 10^{-5}} = 1.33 \times 10^5$. Too low. Use $C_D = 0.5$:

$$0.381 = \frac{1}{2} \times 1.21 V^2 \rho \times 0.4^2 \times 0.5. \quad \therefore V = \underline{1.58 \text{ m/s}}$$

b) $F_D = 2.16 / \tan 70^\circ = 0.786$.

$$0.786 = \frac{1}{2} \times 1.21 V^2 \rho \times 0.4^2 \times 0.2. \quad \therefore V = 3.60 \text{ m/s.}$$

Check Re: $\text{Re} = \frac{3.6 \times 0.8}{1.51 \times 10^{-5}} = 1.9 \times 10^5$. Too low. Use $C_D = 0.5$:

$$0.786 = \frac{1}{2} \times 1.21 V^2 \rho \times 0.4^2 \times 0.5. \quad \therefore V = \underline{2.27 \text{ m/s}}$$

c) $F_D = 2.16 / \tan 60^\circ = 1.25$.

$$1.25 = \frac{1}{2} \times 1.21 V^2 \rho \times 0.4^2 \times 0.5. \quad \therefore V = \underline{2.86 \text{ m/s.}}$$

Check Re: $\text{Re} = \frac{2.86 \times 0.8}{1.51 \times 10^{-5}} = 1.5 \times 10^5$. \therefore OK.

d) $F_D = 2.16 / \tan 50^\circ = 1.81$.

$$1.81 = \frac{1}{2} \times 1.21 V^2 \rho \times 0.4^2 \times 0.5. \quad \therefore V = \underline{3.45 \text{ m/s.}}$$

Check Re: $\text{Re} = \frac{3.45 \times 0.8}{1.51 \times 10^{-5}} = 1.8 \times 10^5$. Close, but OK.

8.36 Assume each section of the tree is a cylinder. The average diameter of the tree is 1 m. The top doesn't have a blunt end around which the air flows, however,

the bottom does; so assume $L/D = (5/2) \times 2 = 5$. So, use a factor of 0.62 from Table 8.1 to multiply the drag coefficient. The force acts near the centroid of the triangular area, one-third the way up. Finally,

$$F \times d = 5000$$

$$\left[\frac{1}{2} \times 1.21 V^2 (5) \times 0.4 \times 0.62 \right] \times \left(\frac{5}{3} + 0.6 \right) = 5000. \quad V = \underline{54.2 \text{ m/s.}}$$

8.37 Power to move the sign:

$$F_D V = \frac{1}{2} \rho V^2 A C_D \times V$$

$$= \frac{1}{2} \times 1.21 \times 11.11^2 \times 0.72 \times 1.1 \times 11.11 = 657 \text{ J/s.}$$

This power comes from the engine:

$$657 = (12\,000 \times 1000) \dot{m} \times 0.3. \quad \therefore \dot{m} = 1.825 \times 10^{-4} \text{ kg/s.}$$

Assuming the density of gas to be 900 kg/m³,

$$1.825 \times 10^{-4} \times 10 \times 3600 \times 6 \times 52 \times \frac{1000}{900} \times 0.30 = \underline{\$683}$$

8.38 The power expended is $F_D \times V$. $V = (25 \times 88 / 60) / 3.281 = 11.18 \text{ m/s}$

$$\frac{1}{2} \rho \cdot 1.21 \cdot 11.18^3 \cdot 0.56 \cdot C_D = \frac{1}{2} \rho \cdot 1.21 \cdot V^3 \cdot 0.4 \cdot C_D \cdot 0.8$$

$$\therefore V = 13.47 \text{ m/s or } \underline{30.1 \text{ mph.}}$$

8.39 $\dot{W} = 40 \times 746 \text{ h} = F_D \times V = \frac{1}{2} \rho V^2 A C_D \times V = \frac{1}{2} \rho A C_D V^3$.

$$\therefore 40 \times 746 \times 9 = \frac{1}{2} \times 1.22 \times 3 \times 0.35 V^3. \quad \therefore V = 34.7 \text{ m/s or } \underline{125 \text{ km/hr.}}$$

8.40 (C) $\text{Re} = \frac{VD}{\nu} = \frac{4 \times 0.02}{1.6 \times 10^{-5}} = 5000. \quad \therefore \text{St} = 0.21 = \frac{fD}{V} = \frac{f \times 0.02}{4}$.

$$\therefore f = 42 \text{ Hz (cycles/second). distance} = \frac{V}{f} = \frac{4 \text{ m/s}}{42 \text{ cycles/s}} = 0.095 \text{ m/cycle.}$$

8.41 $40 < \text{Re} < 10\,000. \quad 40 < \frac{V \times .003}{1.5 \times 10^{-5}} < 10\,000. \quad \therefore \underline{0.2 < V < 50 \text{ m/s.}}$

$$\text{St} = 0.12 = \frac{f \times .003}{.2}. \quad \therefore f_{\text{low}} = 8 \text{ Hz.}$$

$$\text{St} = .21 = \frac{f \times .003}{50}. \quad \therefore f_{\text{high}} = 3500 \text{ Hz.}$$

The vortices could be heard over most of the range.

$$8.42 \quad 40 > \frac{VD}{n} = \frac{6D}{1.22 \times 10^{-5}}. \quad \therefore D < 8.13 \times 10^{-5} \text{ ft.}$$

$$10\,000 < \frac{VD}{n} = \frac{6D}{1.22 \times 10^{-5}}. \quad \therefore D > 0.020 \text{ ft or } \underline{0.24"}$$

$$8.43 \quad \text{From Fig. 8.9, Re is related to St. } St = \frac{f \times D}{V} = \frac{0.2 \times 1}{V}$$

$$Re = \frac{VD}{n} = \frac{V \times 1}{1.5 \times 10^{-5}}. \quad \text{Try St} = .21: V = 0.095 \text{ m/s. } \therefore Re = 630.$$

This is acceptable. $\therefore V = \underline{0.095 \text{ m/s}}$.

$$8.44 \quad St = \frac{fD}{V} = \frac{.002 \times 2}{V}. \quad Re = \frac{VD}{n} = \frac{V \times 2}{10^{-6}}. \quad \text{Use Fig. 8.9.}$$

Try St = 0.21: $V = \underline{.0191 \text{ m/s}}$. $Re = 38 \times 10^3$. $\therefore \text{OK}$.

8.45 Let $S_f = 0.21$ for the wind imposed vortices. When this frequency equals the natural frequency, or one of its odd harmonics, resonance occurs:

$$f = \sqrt{T / rL^2 d^2 p}$$

$$\frac{0.21 \times 10}{0.016} = \sqrt{30\,000 / 7850 L^2 \times 0.016^2 \times p}. \quad \therefore L = \underline{0.525 \text{ m}}$$

Consider the third and fifth harmonics:

$$f = 3\sqrt{T / rL^2 d^2 p}. \quad \therefore L = \underline{1.56 \text{ m}}$$

$$f = 5\sqrt{T / rL^2 d^2 p}. \quad \therefore L = \underline{2.62 \text{ m}}$$

8.46 (C) By reducing the separated flow area, the pressure in that area increases thereby reducing that part of the drag due to pressure.

Fig. 8.8 Table 8.1

$$8.47 \quad Re = \frac{88 \times 6 / 12}{1.6 \times 10^{-4}} = 2.8 \times 10^5. \quad F_D = \frac{1}{2} \times .00238 \times 88^2 \times 1.0 \times .8 \times \left(6 \times \frac{6}{12}\right) = 22 \text{ lb.}$$

The coefficient 1.0 comes from Fig. 8.8 and 0.8 from Table 8.1.

$$\dot{W} = F_D \times V = 22 \times 88 = 1946 \text{ ft} \cdot \text{lb} / \text{sec} \quad \text{or} \quad \underline{3.5 \text{ Hp.}}$$

$$(C_D)_{\text{streamlined}} = 0.035. \quad \therefore F_D = 0.77 \text{ lb.} \quad \dot{W} = 67.8 \frac{\text{ft} \cdot \text{lb}}{\text{sec}} \quad \text{or} \quad \underline{0.12 \text{ Hp.}}$$

$$8.48 \quad Re = \frac{VD}{n} = \frac{3 \times .08}{1.5 \times 10^{-5}} = 16\,000. \quad \therefore F_D = \frac{1}{2} \times 1.22 \times 3^2 \times (0.08 \times 2) \times 1.2 \times .78 = \underline{0.822 \text{ N}}$$

The coefficient 1.2 comes from Fig. 8.8 and 0.78 from Table 8.1.

$$(C_D)_{\text{streamlined}} = .35. \quad \therefore F_D = 0.24 \text{ N.} \quad \therefore \% \text{ reduction} = \frac{0.822 - 0.24}{0.822} \times 100 = \underline{70.8\%}$$

$$8.49 \quad \text{Re} = \frac{VD}{\nu} = \frac{2 \times 0.8}{10^{-6}} = 1.6 \times 10^6. \quad \therefore C_D = 0.45 \text{ from Fig. 8.8.}$$

$$\frac{L}{D} = \frac{4}{0.8} = 5. \quad \therefore C_D = 0.62 \times 0.45 = 0.28.$$

Because only one end is free, we double the length.

$$F_D = \frac{1}{2} \rho V^2 A C_D = \frac{1}{2} \times 1000 \times 2^2 \times 0.8 \times 2 \times 0.28 = \underline{900 \text{ N}}.$$

If streamlined, $C_D = 0.03 \times 0.62 = 0.0186$.

$$\therefore F_D = \frac{1}{2} \times 1000 \times 2^2 \times 0.8 \times 2 \times 0.0186 = \underline{60 \text{ N}}.$$

$$8.50 \quad V = 50 \times 1000 / 3600 = 13.9 \text{ m / s.}$$

Assume the ends to not be free. \therefore Use C_D from Fig. 8.8.

$$\text{Re} = \frac{13.9 \times 0.02}{1.5 \times 10^{-5}} = 1.85 \times 10^4. \quad \therefore C_D = 1.2. \quad (C_D)_{\text{streamlined}} = 0.3$$

$$\dot{W} = F_D \times V = \frac{1}{2} \rho V^3 A C_D = \frac{1}{2} \times 1.2 \times 13.9^3 \times 0.02 \times 20 \times 1.2 = 773 \text{ W or } \underline{1.04 \text{ Hp}}.$$

$$\dot{W}_{\text{streamlined}} = \frac{1}{2} \times 1.2 \times 13.9^3 \times 0.02 \times 20 \times 0.3 = 193 \text{ W or } \underline{0.26 \text{ Hp}}$$

$$8.51 \quad V = 50 \times 1000 / 3600 = 13.9 \text{ m / s.} \quad \text{Re} = \frac{13.9 \times 0.3}{1.5 \times 10^{-5}} = 2.8 \times 10^5. \quad \therefore C_D = 0.4$$

We assumed a head diameter of 0.3 m and used the rough sphere curve.

$$F_D = \frac{1}{2} \times 1.2 \times 13.9^2 (\rho \times 0.3^2 / 4) \times 0.4 = \underline{3.3 \text{ N}}.$$

$$F_D = \frac{1}{2} \times 1.2 \times 13.9^2 (\rho \times 0.3^2 / 4) \times 0.035 = \underline{0.29 \text{ N}}.$$

$$8.52 \quad s = \frac{p_\infty - p_v}{\frac{1}{2} \rho V^2}. \quad 0.7 = \frac{150\,000 - 1670}{\frac{1}{2} \times 1000 V^2} \quad \text{where } p_\infty = \rho g h + p_{\text{atm}} = 150\,000 \text{ Pa.}$$

$$\therefore V = \underline{20.6 \text{ m / s.}}$$

$$8.53 \quad C_L = \frac{F_L}{\frac{1}{2} \rho V^2 A} = \frac{200\,000}{\frac{1}{2} \times 1000 \times 12^2 \times 4 \times 10} = 0.69. \quad \therefore \alpha \cong 3^\circ.$$

$$C_D = .0165 = \frac{F_D}{\frac{1}{2} \times 1000 \times 12^2 \times 4 \times 10}. \quad \therefore F_D = \underline{4800 \text{ N}}.$$

$$s_{\text{crit}} = .75 \stackrel{?}{>} \frac{(9810 \times 4 + 101\,000) - 1670}{\frac{1}{2} \times 1000 \times 12^2} = 1.43. \quad \therefore \underline{\text{No cavitation.}}$$

$$8.54 \quad C_L = \frac{F_L}{\frac{1}{2} \rho V^2 A} = \frac{50\,000}{\frac{1}{2} \times 1.94 \times 35^2 \times \frac{16}{12} \times 30} = 1.05. \quad \therefore \mathbf{a} = 7.3^\circ.$$

$$C_D = .027 = \frac{F_D}{\frac{1}{2} \times 1.94 \times 35^2 \times \frac{16}{12} \times 30}. \quad \therefore F_D = \underline{1280 \text{ lb.}}$$

$$s_{\text{crit}} = 1.6 \stackrel{?}{>} \frac{62.4 \times 16 / 12 + 2117 - .25 \times 144}{\frac{1}{2} \times 1.94 \times 35^2} = 1.82. \quad \therefore \underline{\text{No cavitation.}}$$

$$8.55 \quad p_\infty = 9810 \times 5 + 101\,000 = 150\,000 \text{ Pa.} \quad p_v = 1670 \text{ Pa.} \quad \text{Re} = \frac{20 \times 8}{10^{-6}} = 16 \times 10^6.$$

$$s = \frac{150\,000 - 1670}{\frac{1}{2} \times 1000 \times 20^2} = 0.74. \quad \therefore C_D = C_D(0)(1 + s) = .3(1 + .74) = .52$$

$$\therefore F_D = \frac{1}{2} \rho V^2 A C_D = \frac{1}{2} \times 1000 \times 20^2 \times \rho \times .4^2 \times .52 = \underline{52\,000 \text{ N.}}$$

Note: We retain 2 sig. figures since C_D is known to only 2 sig. nos.

8.56 For a 6° angle of attack we find from Table 8.4 $C_L = 0.95$.

$$F_L = \frac{1}{2} \rho V^2 A C_L = \frac{1}{2} \times 1000 \times 15^2 \times 4 \times 0.4 L \times .95 = 12\,000 \times 9.8.$$

$$\therefore L = \underline{0.69 \text{ m.}}$$

$$8.57 \quad \Sigma F = ma \quad \text{a) } 400 - 9810 \times \frac{4}{3} \rho \times .2^3 = \frac{400}{9.81} a \quad \therefore a = \underline{1.75 \text{ m/s}^2}.$$

$$\text{b) } 400 - 9810 \times \frac{4}{3} \rho \times .2^3 = \left(\frac{400}{9.81} + \frac{1}{2} \times 1000 \times \frac{4}{3} \rho \times .2^3 \right) a \quad \therefore a = \underline{1.24 \text{ m/s}^2}.$$

$$8.58 \quad F = m a_1 = 1000 \times 1.2 \times V a_1. \quad \therefore a_1 = \frac{F}{1200 V}. \quad m_a = 0.2 \times 1000 V.$$

$$F = (m + m_a) a_2. \quad \therefore a_2 = \frac{F}{1200 V + 200 V} = \frac{F}{1400 V}. \quad a_2 \text{ is true acceleration.}$$

$$\therefore \% \text{ error} = \left| \frac{a_2 - a_1}{a_2} \right| \times 100 = \left| \frac{\frac{F}{1400 V} - \frac{F}{1200 V}}{\frac{F}{1400 V}} \right| \times 100 = \underline{16.7\%}$$

8.59 (B) From Fig. 8.12a $C_L = 1.1$. $C_L = \frac{F_L}{\frac{1}{2}\rho V^2 c_L}$.

$$\therefore V^2 = \frac{2W}{\rho c_L C_L} = \frac{2 \times 1200 \times 9.81}{1.23 \times 16 \times 1.1} = 1088. \quad \therefore V = 33.0 \text{ m/s.}$$

8.60 $C_L = \frac{F_L}{\frac{1}{2}\rho V^2 A} = \frac{1000 \times 9.81}{\frac{1}{2} \times .412 \times 80^2 \times 15} = 0.496. \quad \therefore \alpha = 3.2^\circ. \quad C_D = .0065.$

$$\dot{W} = F_D V = \left(\frac{1}{2} \times .412 \times 80^2 \times 15 \times .0065 \right) \times 80 = 10\,300 \text{ W or } \underline{13.8 \text{ Hp.}}$$

8.61 a) $C_L = 1.22 = \frac{1500 \times 9.81 + 3000}{\frac{1}{2} \times 1.22 \times V^2 \times 20}. \quad \therefore V = \underline{34.5 \text{ m/s.}}$

b) $(C_L)_{\max} = 1.72 = \frac{1500 \times 9.81 + 3000}{\frac{1}{2} \times .412 \times V^2 \times 20}. \quad \therefore V = \underline{50 \text{ m/s.}} \quad (\text{at } 10\,000 \text{ m})$

c) $\dot{W} = F_D V = \left(\frac{1}{2} \times .412 \times 80^2 \times 20 \times .0065 \right) \times 80 = 13\,700 \text{ W or } \underline{18.4 \text{ Hp}}$

where we found C_D as follows:

$$(C_L)_{\text{cruise}} = \frac{1500 \times 9.81 + 3000}{\frac{1}{2} \times .412 \times 80^2 \times 20} = .67. \quad \therefore C_D = .0065, \text{ from Fig. 8.12.}$$

$$\therefore \text{Power} = \frac{18.4}{0.45} = \underline{40.9 \text{ Hp.}}$$

8.62 $C_L = 1.22 = \frac{1500 \times 9.81 + 3000}{\frac{1}{2} \times 1.007 \times V^2 \times 20}. \quad \therefore V = \underline{38.0 \text{ m/s.}}$

8.63 $(C_L)_{\text{cruise}} = \frac{1500 \times 9.81 + 3000}{\frac{1}{2} \times 1.007 \times 80^2 \times 20} = 0.275. \quad \therefore C_D = \frac{0.275}{48} = 0.0057.$

$$\therefore \dot{W} = F_D V = \frac{1}{2} \times 1.007 \times 80^3 \times 20 \times 0.0057 = 29\,400 \text{ W or } 39.4 \text{ Hp}$$

$$\% \text{ change} = \frac{39.4 - 18.4}{18.4} \times 100 = \underline{114\% \text{ increase}}$$

The increased power is due to the increase in air density.

$$8.64 \quad C_L = 1.22 = \frac{1500 \times 9.81 + 9000}{\frac{1}{2} \times 1.22 \times V^2 \times 20} \quad \therefore V = \underline{39.9 \text{ m/s}}$$

$$8.65 \quad C_L = 1.72 = \frac{250\,000 \times 9.81}{\frac{1}{2} \times 1.22 \times V^2 \times 60 \times 8} \quad \therefore V = \underline{69.8 \text{ m/s}}$$

$$8.66 \quad \text{a) } C_L = 1.72 = \frac{250\,000 \times 9.81}{\frac{1}{2} \times 1.05 \times V^2 \times 60 \times 8} \quad \therefore V = 75.2 \text{ m/s}$$

$$\% \text{ change} = \frac{75.2 - 69.8}{69.8} \times 100 = \underline{7.77\% \text{ increase}}$$

$$\text{b) } C_L = 1.72 = \frac{250\,000 \times 9.81}{\frac{1}{2} \times 1.515 V^2 \times 60 \times 8} \quad \therefore V = 62.6 \text{ m/s} \quad \left(\mathbf{r} = \frac{101.3}{.287 \times 233} = 1.515 \text{ kg/m}^3 \right)$$

$$\% \text{ change} = \frac{62.6 - 69.8}{69.8} \times 100 = \underline{-10.3\%}$$

$$\text{c) } C_L = 1.72 = \frac{250\,000 \times 9.81}{\frac{1}{2} \times 1.093 V^2 \times 60 \times 8} \quad \therefore V = 73.7 \text{ m/s} \quad \left(\mathbf{r} = \frac{101.3}{.287 \times 323} = 1.093 \text{ kg/m}^3 \right)$$

$$\% \text{ change} = \frac{73.7 - 69.8}{69.8} \times 100 = \underline{5.63\% \text{ increase}}$$

8.67 For a conventional airfoil assume $C_L / C_D = 47.6$ at $C_L = 0.3$.

$$0.3 = \frac{m \times 9.81}{\frac{1}{2} \times 0.526 \times 222^2 \times 200 \times 30} \quad \therefore m = \underline{2.38 \times 10^6 \text{ kg}}$$

$$\dot{W} = F_D V = \frac{1}{2} \times 0.526 \times 222^3 \times 200 \times 30 \times \frac{0.3}{47.6} = 490\,000 \text{ W or } \underline{657 \text{ Hp}}$$

$$8.68 \quad \bar{\nabla} \times \left[\frac{\mathcal{I} \bar{V}}{\mathcal{I} t} + (\bar{V} \cdot \bar{\nabla}) \bar{V} + \frac{\bar{\nabla} p}{\mathbf{r}} - \mathbf{n} \nabla^2 \bar{V} \right] = 0.$$

$$\bar{\nabla} \times \frac{\mathcal{I} \bar{V}}{\mathcal{I} t} = \frac{\mathcal{I}}{\mathcal{I} t} (\bar{\nabla} \times \bar{V}) = \frac{\mathcal{I} \bar{\omega}}{\mathcal{I} t} \quad \bar{\nabla} \times \frac{\bar{\nabla} p}{\mathbf{r}} = \frac{1}{\mathbf{r}} \bar{\nabla} \times \bar{\nabla} p = 0.$$

$$\bar{\nabla} \times (\nabla^2 \bar{V}) = \nabla^2 (\bar{\nabla} \times \bar{V}) = \nabla^2 \bar{\omega} \quad (\text{we have interchanged derivatives})$$

$$\begin{aligned} \bar{\nabla} \times [(\bar{V} \cdot \bar{\nabla}) \bar{V}] &= \bar{\nabla} \times \left[\frac{1}{2} \bar{\nabla} V^2 - \bar{V} \times (\bar{\nabla} \times \bar{V}) \right] = \frac{1}{2} (\bar{\nabla} \times \bar{\nabla} V^2) - \bar{\nabla} \times (\bar{V} \times \bar{\omega}) \\ &= \bar{V} (\bar{\nabla} \cdot \bar{\omega}) - \bar{\omega} (\bar{\nabla} \cdot \bar{V}) + (\bar{V} \cdot \bar{\nabla}) \bar{\omega} - (\bar{\omega} \cdot \bar{\nabla}) \bar{V} \end{aligned}$$

$$x=L, u=U. \quad \therefore \frac{\mathcal{I}y}{\mathcal{I}y} = U. = (\bar{V} \cdot \bar{\nabla})\bar{w} - (\bar{w} \cdot \bar{\nabla})\bar{V} \quad \text{where } \bar{\nabla} \cdot \bar{w} = \bar{\nabla} \cdot (\bar{\nabla} \times \bar{V}) = 0.$$

$$\text{There results:} \quad \frac{\mathcal{I}\bar{w}}{\mathcal{I}t} + (\bar{V} \cdot \bar{\nabla})\bar{w} - (\bar{w} \cdot \bar{\nabla})\bar{V} - \mathbf{n}\nabla^2\bar{w} = 0.$$

$$\text{This is written as} \quad \frac{D\bar{w}}{Dt} = (\bar{w} \cdot \bar{\nabla})\bar{V} + \mathbf{n}\nabla^2\bar{w}.$$

$$8.69 \quad \text{x-comp:} \quad \frac{\mathcal{I}w_x}{\mathcal{I}t} + u \frac{\mathcal{I}w_x}{\mathcal{I}x} + v \frac{\mathcal{I}w_x}{\mathcal{I}y} + w \frac{\mathcal{I}w_x}{\mathcal{I}z} = w_x \frac{\mathcal{I}u}{\mathcal{I}x} + w_y \frac{\mathcal{I}u}{\mathcal{I}y} + w_z \frac{\mathcal{I}u}{\mathcal{I}z} + \mathbf{n}\nabla^2 w_x$$

y-comp:

$$\frac{\mathcal{I}w_y}{\mathcal{I}t} + u \frac{\mathcal{I}w_y}{\mathcal{I}x} + v \frac{\mathcal{I}w_y}{\mathcal{I}y} + w \frac{\mathcal{I}w_y}{\mathcal{I}z} = w_x \frac{\mathcal{I}v}{\mathcal{I}x} + w_y \frac{\mathcal{I}v}{\mathcal{I}y} + w_z \frac{\mathcal{I}v}{\mathcal{I}z} + \mathbf{n} \left(\frac{\mathcal{I}^2 w_y}{\mathcal{I}x^2} + \frac{\mathcal{I}^2 w_y}{\mathcal{I}y^2} + \frac{\mathcal{I}^2 w_y}{\mathcal{I}z^2} \right)$$

z-comp:

$$\frac{\mathcal{I}w_z}{\mathcal{I}t} + u \frac{\mathcal{I}w_z}{\mathcal{I}x} + v \frac{\mathcal{I}w_z}{\mathcal{I}y} + w \frac{\mathcal{I}w_z}{\mathcal{I}z} = w_x \frac{\mathcal{I}w}{\mathcal{I}x} + w_y \frac{\mathcal{I}w}{\mathcal{I}y} + w_z \frac{\mathcal{I}w}{\mathcal{I}z} + \mathbf{n} \left(\frac{\mathcal{I}^2 w_z}{\mathcal{I}x^2} + \frac{\mathcal{I}^2 w_z}{\mathcal{I}y^2} + \frac{\mathcal{I}^2 w_z}{\mathcal{I}z^2} \right)$$

$$8.70 \quad w_x = \frac{\mathcal{I}v}{\mathcal{I}y} - \frac{\mathcal{I}u}{\mathcal{I}z} = 0. \quad w_y = \frac{\mathcal{I}u}{\mathcal{I}z} - \frac{\mathcal{I}v}{\mathcal{I}x} = 0. \quad w_z = \frac{\mathcal{I}v}{\mathcal{I}x} - \frac{\mathcal{I}u}{\mathcal{I}y} \neq 0.$$

$$\frac{Dw_z}{Dt} = (\bar{w} \cdot \bar{\nabla})w + \mathbf{n}\nabla^2 w_z \quad ; \quad \therefore \frac{Dw_z}{Dt} = \mathbf{n}\nabla^2 w_z.$$

$$\text{If viscous effects are negligible, then } \frac{Dw_z}{Dt} = 0.$$

Thus, for a planer flow, $w_z = \text{const}$ if viscous effects are negligible.

$$8.71 \quad \text{a) } \bar{\nabla} \times \bar{V} = \left(\frac{\mathcal{I}w}{\mathcal{I}y} - \frac{\mathcal{I}v}{\mathcal{I}z} \right) \hat{i} + \left(\frac{\mathcal{I}u}{\mathcal{I}z} - \frac{\mathcal{I}w}{\mathcal{I}x} \right) \hat{j} + \left(\frac{\mathcal{I}v}{\mathcal{I}x} - \frac{\mathcal{I}u}{\mathcal{I}y} \right) \hat{k} = 0. \quad \therefore \underline{\text{irrotational}}$$

$$\frac{\mathcal{I}f}{\mathcal{I}x} = 10x. \quad \therefore f = 5x^2 + f(y)$$

$$\frac{\mathcal{I}f}{\mathcal{I}y} = \frac{\mathcal{I}f}{\mathcal{I}y} = 20y. \quad \therefore f = 10y^2 + C. \quad \text{Let } C=0. \quad \therefore \underline{f = 5x^2 + 10y^2}$$

$$\text{b) } \bar{\nabla} \times \bar{V} = 0\hat{i} + 0\hat{j} + (8-8)\hat{k} = 0. \quad \therefore \underline{\text{irrotational}}$$

$$\frac{\mathcal{I}f}{\mathcal{I}x} = 8y. \quad \therefore f = 8xy + f(y, z). \quad \frac{\mathcal{I}f}{\mathcal{I}y} = 8x + \frac{\mathcal{I}f}{\mathcal{I}y} = 8x. \quad \therefore \frac{\mathcal{I}f}{\mathcal{I}y} = 0 \text{ and } f = f(z).$$

$$\frac{\mathcal{I}f}{\mathcal{I}z} = \frac{df}{dz} = -6z. \quad \therefore f = -3z^2 + C. \quad \text{Let } C=0.$$

$$\therefore \underline{f = 8xy - 3z^2}$$

$$c) \bar{\nabla} \times \bar{V} = 0\hat{i} + 0\hat{j} + \left(\frac{-y \frac{1}{2}(x^2 + y^2)^{-1/2} 2x}{x^2 + y^2} - \frac{-x \frac{1}{2}(x^2 + y^2)^{-1/2} 2y}{x^2 + y^2} \right) \hat{k} = 0. \quad \therefore \underline{\text{irrotational}}$$

$$\frac{\partial f}{\partial x} = \frac{x}{\sqrt{x^2 + y^2}}. \quad \therefore f = \sqrt{x^2 + y^2} + f(y)$$

$$\frac{\partial f}{\partial y} = \frac{1}{2}(x^2 + y^2)^{-1/2} 2y + \frac{\partial f}{\partial y} = \frac{y}{\sqrt{x^2 + y^2}}. \quad \therefore \frac{\partial f}{\partial y} = 0. \quad \therefore f = C. \quad \text{Let } C = 0.$$

$$\therefore \underline{f = \sqrt{x^2 + y^2}}$$

$$d) \bar{\nabla} \times \bar{V} = 0\hat{i} + 0\hat{j} + \left[\frac{-y(2x)}{(x^2 + y^2)^2} - \frac{-x(2y)}{(x^2 + y^2)^2} \right] \hat{k} = 0. \quad \therefore \underline{\text{irrotational}}$$

$$\frac{\partial f}{\partial x} = \frac{x}{x^2 + y^2}. \quad \therefore f = \frac{1}{2} \ln(x^2 + y^2) + f(y)$$

$$\frac{\partial f}{\partial y} = \frac{y}{x^2 + y^2} = \frac{1}{2} \frac{2y}{x^2 + y^2} + \frac{\partial f}{\partial y}. \quad \therefore \frac{\partial f}{\partial y} = 0. \quad \therefore f = C. \quad \text{Let } C = 0.$$

$$\therefore \underline{f = \ln \sqrt{x^2 + y^2}}$$

$$8.72 \quad \frac{\partial^2 y}{\partial x^2} + \frac{\partial^2 y}{\partial y^2} = 0. \quad \text{This requires two conditions on } x \text{ and two on } y.$$

$$\text{At } x = -L, \quad u = U. \quad \therefore \frac{\partial y}{\partial y} = U.$$

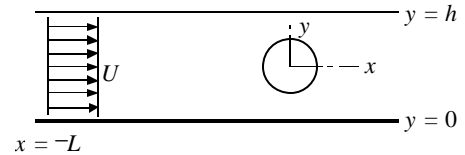
$$\text{At } x = L, \quad u = U. \quad \therefore \frac{\partial y}{\partial y} = U.$$

$$\text{At } y = -h, \quad y = 0.$$

$$\text{At } y = h, \quad y = U \times h. \quad (\text{See Example 8.9}).$$

The boundary conditions are stated as:

$$\frac{\partial y}{\partial y}(-L, y) = U, \quad \frac{\partial y}{\partial y}(L, y) = U, \quad y(x, -h) = 0, \quad y(x, h) = 2Uh.$$



$$8.73 \quad u = \frac{\partial y}{\partial y} = 100. \quad \therefore y = 100y + f(x). \quad v = -\frac{\partial y}{\partial x} = -\frac{df}{dx} = 50. \quad \therefore f = -50x + C.$$

$$\therefore \underline{y(x, y) = 100y - 50x.} \quad (\text{We usually let } C = 0.)$$

$$u = \frac{\partial f}{\partial x} = 100. \quad \therefore f = 100x + f(y). \quad v = \frac{\partial f}{\partial y} = \frac{df}{dy} = 50. \quad \therefore f = 50y + C.$$

$$\therefore \underline{f(x, y) = 100x + 50y.}$$

8.74 a) $y = 40q$.

b) $\frac{1}{r} \frac{\partial}{\partial r} \left(\frac{\partial y}{\partial r} \right) + \frac{1}{r} \left(-\frac{\partial^2 y}{\partial q \partial r} \right) = \frac{1}{r} \frac{\partial}{\partial r} (40) + \frac{1}{r} \left(-\frac{\partial}{\partial q} (0) \right) = 0$.

∴ It is incompressible since the above continuity equation is satisfied.

Note: The continuity equation is found in Table 5.1.

c) $\frac{\partial f}{\partial r} = \frac{1}{r} \frac{\partial y}{\partial q} = \frac{40}{r}$. ∴ $f = 40 \ln r + f(q)$

$\frac{\partial f}{\partial q} = \frac{\partial f}{\partial q} = -r \frac{\partial y}{\partial r} = 0$. ∴ $f = C$. Let $C = 0$.

∴ $f = 40 \ln r$

d) $v_r = \frac{40}{r}$, $v_q = 0$. $a_r = v_r \frac{\partial v_r}{\partial r} = \frac{40}{r} \left(-\frac{40}{r^2} \right) = -10$.

∴ $r = 5.43 \text{ m}$

8.75 $u = \frac{\partial y}{\partial y} = 20 \frac{2y}{x^2 + y^2} = \frac{\partial f}{\partial x}$. ∴ $f = -40 \tan^{-1} \frac{y}{x} + f(y)$.

$v = \frac{\partial f}{\partial y} = -\frac{40/x}{1 + y^2/x^2} + \frac{\partial f}{\partial y} = -\frac{40x}{x^2 + y^2} + \frac{\partial f}{\partial y} = -20 \frac{2x}{x^2 + y^2}$. ∴ $f = C$. Let $C = 0$.

$f = -40 \tan^{-1} \frac{y}{x}$.

8.76 a) $\frac{\partial^2 y}{\partial x^2} + \frac{\partial^2 y}{\partial y^2} = 0$. $\frac{\partial y}{\partial x} = 10y(x^2 + y^2)^{-2} (2x)$.

$\frac{\partial^2 y}{\partial x^2} = 20y(x^2 - y^2)^{-2} - 80x^2 y(x^2 + y^2)^{-3}$

$\frac{\partial y}{\partial y} = 10 - 10(x^2 + y^2)^{-1} + 10y(x^2 + y^2)^{-2} (2y)$.

$\frac{\partial^2 y}{\partial y^2} = 20y(x^2 + y^2)^{-2} + 40y(x^2 + y^2)^{-2} - 80y^3(x^2 + y^2)^{-3}$.

∴ $\frac{\partial^2 y}{\partial x^2} + \frac{\partial^2 y}{\partial y^2} = \frac{20y}{(x^2 + y^2)^2} - \frac{80x^2 y}{(x^2 + y^2)^3} + \frac{60y}{(x^2 + y^2)^2} - \frac{80y^3}{(x^2 + y^2)^3}$
 $= \frac{80y(x^2 + y^2)}{(x^2 + y^2)^3} - \frac{80x^2 y}{(x^2 + y^2)^3} - \frac{80y^3}{(x^2 + y^2)^3} = \frac{80x^2 y + 80y^3 - 80x^2 y - 80y^3}{(x^2 + y^2)^3} = 0$.

b) In polar coord: $y(r, q) = 10r \sin q - \frac{10r \sin q}{r^2} = 10r \sin q - \frac{10}{r} \sin q$.

$\frac{1}{r} \frac{\partial y}{\partial q} = \left(10 - \frac{10}{r^2} \right) \cos q = \frac{\partial f}{\partial r}$. ∴ $f = \left(10 + \frac{10}{r} \right) \cos q + f(q)$.

$$\frac{1}{r} \frac{\partial f}{\partial r} = \frac{1}{r} \frac{df}{dq} - \left(10 + \frac{10}{r^2}\right) \sin q = -\frac{\partial y}{\partial r} = -10 \sin q - \frac{10}{r^2} \sin q. \quad \frac{df}{dq} = 0. f = \text{const.}$$

$$\therefore f = 10 \left(r + \frac{1}{r} \right) \cos q \quad \text{or} \quad f(x, y) = 10x + \frac{10x}{x^2 + y^2},$$

where we let $r \cos q = x$ and $r^2 = x^2 + y^2$.

c) Along the x -axis, $v = -\frac{\partial y}{\partial x} = 0$ where we let $y = 0$ in part (a) and

$$u = \frac{\partial y}{\partial y} = 10 - \frac{10}{x^2 + y^2} + \frac{20y^2}{(x^2 + y^2)^2} = 10 - \frac{10}{x^2} \quad \text{with } y = 0.$$

$$\text{Euler's Eq: } ru \frac{\partial u}{\partial x} = -\frac{\partial p}{\partial x}. \quad \therefore r \left(10 - \frac{10}{x^2} \right) \left(\frac{20}{x^3} \right) = -\frac{\partial p}{\partial x}.$$

$$\therefore p = \int r \left(\frac{200}{x^5} - \frac{200}{x^3} \right) dx = r \left[-\frac{50}{x^4} + \frac{100}{x^2} \right] + C. \quad C = 50\,000.$$

$$= 1000 \left[\frac{100}{x^2} - \frac{50}{x^4} \right] + 50\,000 \text{ Pa.} \quad (\text{Could have used Bernoulli!})$$

d) Let $u = 0$: $0 = 10 - \frac{10}{x^2}$. $\therefore x = \pm 1$. \therefore Stag pts: (1, 0), (-1, 0)

8.77 a) $\frac{\partial^2 f}{\partial x^2} + \frac{\partial^2 f}{\partial y^2} = \frac{\partial}{\partial x} \left[10 + \frac{10x}{x^2 + y^2} \right] + \frac{\partial}{\partial y} \left[\frac{10y}{x^2 + y^2} \right] = \frac{(x^2 + y^2)10 - 10x(2x)}{(x^2 + y^2)^2} + \frac{(x^2 + y^2)10 - 10y(2y)}{(x^2 + y^2)^2} = \frac{10x^2 + 10y^2 - 20x^2 + 10x^2 + 10y^2 - 20y^2}{(x^2 + y^2)^2} = 0.$

b) Polar coord: $f = 10r \cos q + 5 \ln r^2$. (See Eq. 8.5.14.)

$$\frac{\partial f}{\partial r} = 10 \cos q + \frac{10r}{r^2} = \frac{1}{r} \frac{\partial y}{\partial q}. \quad \therefore y = 10r \sin q + 10q + f(r)$$

$$\frac{1}{r} \frac{\partial f}{\partial q} = -10 \sin q = -\frac{\partial y}{\partial r} = -10 \sin q - \frac{df}{dr}. \quad \therefore f = \text{const.} \quad \therefore y = 10r \sin q + 10q.$$

$$\therefore y(x, y) = 10y + 10 \tan^{-1} \frac{y}{x}.$$

c) $v = \frac{\partial f}{\partial y} = \frac{10y}{x^2 + y^2}$. Along x -axis ($y = 0$) $v = 0$.

$$u = \frac{\partial f}{\partial x} = 10 + \frac{10x}{x^2 + y^2}. \quad \text{Along } x\text{-axis } u = 10 + \frac{10}{x}.$$

$$\text{Bernoulli: } \frac{V^2}{2} + \frac{p}{\rho} + gz = \frac{V_\infty^2}{2} + \frac{p_\infty}{\rho} + gz_\infty \quad (\text{assume } z = z_\infty)$$

$$\frac{(10 + 10/x)^2}{2} + \frac{p}{\rho} = \frac{10^2}{2} + \frac{100\,000}{\rho}. \quad \therefore p = 100 - 50 \left(\frac{2}{x} + \frac{1}{x^2} \right) \text{ kPa.}$$

d) $u = 0: \quad 0 = 10 + \frac{10}{x}. \quad \therefore x = -1. \quad \therefore \text{Stag pt: } (-1, 0)$

e) $a_y = \cancel{v} \frac{\cancel{v}}{\cancel{y}} + u \frac{\cancel{y}}{\cancel{x}} = 0$ on x -axis. $a_x = u \frac{\cancel{u}}{\cancel{x}} + \cancel{v} \frac{\cancel{u}}{\cancel{y}} = \left(10 + \frac{10}{x}\right) \left(-\frac{10}{x^2}\right)$
 $\therefore a_x(-2, 0) = (10 - 5) \left(-\frac{10}{4}\right) = -12.5 \text{ m/s}^2$.

8.78 $u(x, y) = y - 5y^2 = \frac{\cancel{y}}{\cancel{y}}. \quad \therefore \mathbf{y} = \frac{y^2}{2} - \frac{5y^3}{3} + \cancel{C}. \quad \therefore \mathbf{y} = \frac{1}{6}(3y^2 - 10y^3)$.

$q = \int_0^{.2} u dy = \int_0^{.2} (y - 5y^2) dy = \frac{0.2^2}{2} - 5 \frac{0.2^3}{3} = 6.667 \times 10^{-3} \text{ m}^2/\text{s}$.

$y_2 - y_1 = \frac{1}{6}(3 \times 0.2^2 - 10 \times 0.2^3) - 0 = 6.667 \times 10^{-3} \text{ m}^2/\text{s}$.

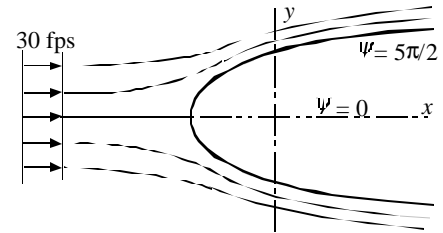
$w = -\frac{\cancel{u}}{\cancel{y}} = -1 + 10y \neq 0. \quad \therefore f$ doesn't exist.

8.79 $\mathbf{y} = 30\mathbf{y} + \frac{5\mathbf{p}}{2\mathbf{p}}\mathbf{q} = 30r \sin \mathbf{q} + \frac{5}{2}\mathbf{q}$.

a) $v_r = \frac{1}{r} \frac{\cancel{y}}{\cancel{q}} = 30 \cos \mathbf{q} + \frac{5}{2r} = 0$.

At $\mathbf{q} = \mathbf{p}, \quad \frac{5}{2r_s} = 30. \quad \therefore r_s = 0.0833'$.

Stag. pt: $(-1'', 0)$.



b) At $\mathbf{q} = \mathbf{p}, \quad r = .0833, \quad y_s = \frac{5\mathbf{p}}{2} = 30r \sin \frac{\mathbf{p}}{2} + \frac{5}{2} \frac{\mathbf{p}}{2}$.

$\therefore r = y_{\text{inter}} = .0119 \text{ ft}$.

c) $q = U \times H = \Delta y. \quad \therefore 30H = \frac{5\mathbf{p}}{2}. \quad \therefore H = \frac{5\mathbf{p}}{60}. \quad \text{Thickness} = 2H = \frac{5\mathbf{p}}{30} \text{ ft or } 1.257''$.

d) $v_r(1, \mathbf{p}) = 30 \cos \mathbf{p} + \frac{5}{2} = -30 + 2.5 = -27.5. \quad \therefore u = 27.5 \text{ fps}$.

8.80 $f = \frac{\mathbf{p}}{2\mathbf{p}} \ln[(x+1)^2 + y^2]^{1/2} - \frac{\mathbf{p}}{2\mathbf{p}} \ln[(x-1)^2 + y^2]^{1/2} + 10x = \frac{1}{4} \ln[(x+1)^2 + y^2]$
 $-\frac{1}{4} \ln[(x-1)^2 + y^2] + 10x$.

$u = \frac{\cancel{f}}{\cancel{x}} \Big|_{y=0} = \frac{1}{4} \frac{[2(x+1)]}{(x+1)^2} - \frac{1}{4} \frac{[2(x-1)]}{(x-1)^2} + 10 = \frac{1}{2(x+1)} - \frac{1}{2(x-1)} + 10. \quad v = 0 \text{ if } y = 0$.

At the stagnation point, $u = 0$. $\therefore \frac{1}{2(x+1)} - \frac{1}{2(x-1)} + 10 = 0$. $\therefore \frac{2}{x^2 - 1} = 20$.

$\therefore x^2 = 1.1$. $\therefore x = \pm 1.049$ m. \therefore oval length = $2 \times 1.049 = \underline{2.098}$ m.

All the flow from the source goes to the sink, i.e., p m² / s, or $\frac{p}{2}$ m² / s for $y > 0$.

$$u(y) = \frac{q}{x} \Big|_{x=0} = \frac{\frac{1}{4}(2)}{1+y^2} - \frac{\frac{1}{4}(-2)}{1+y^2} + 10 = \frac{1}{1+y^2} + 10.$$

$$q = \int_0^h \left(\frac{1}{1+y^2} + 10 \right) dy = \frac{p}{2}. \quad \therefore \tan^{-1} h + 10h = \frac{p}{2}.$$

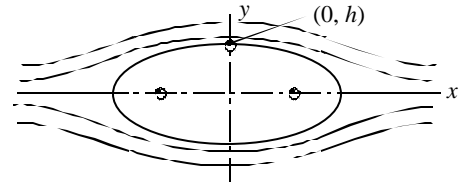
$h = 0.143$ m so that thickness = $2h = \underline{0.286}$ m.

The minimum pressure occurs on the oval surface at $(0, h)$.

There $u = \frac{1}{1+.143^2} + 10 = 10.98$ m / s.

$$\text{Bernoulli: } \frac{V^2}{2} + \frac{p}{\rho} = \frac{V_\infty^2}{2} + \frac{p_\infty}{\rho}. \quad \frac{10.98^2}{2} + \frac{p}{1000} = \frac{10^2}{2} + \frac{10\,000}{1000}.$$

$$\therefore \underline{p_{\min} = -280 \text{ Pa.}}$$



$$8.81 \quad f = \frac{2p}{2p} \ln[(x+1)^2 + y^2]^{1/2} + \frac{-2p}{2p} \ln[(x-1)^2 + y^2]^{1/2} + 2x = \frac{1}{2} \ln[(x+1)^2 + y^2] - \frac{1}{2} \ln[(x-1)^2 + y^2] + 2x.$$

$$u = \frac{q}{x} = \frac{\frac{1}{2}2(x+1)}{(x+1)^2 + y^2} - \frac{\frac{1}{2}2(x-1)}{(x-1)^2 + y^2} + 2. \quad v = \frac{y}{(x-1)^2 + y^2} - \frac{y}{(x+1)^2 + y^2}$$

Along the x -axis ($y = 0$), $v = 0$ and $u = \frac{1}{x+1} - \frac{1}{x-1} + 2$.

Set $u = 0$: $\frac{1}{x-1} - \frac{1}{x+1} = 2$, or $x^2 = 2$. $\therefore x = \pm\sqrt{2}$.

Stag. pts.: $(\sqrt{2}, 0), (-\sqrt{2}, 0)$.

$$u(4, 0) = \frac{1}{-4+1} - \frac{1}{-4-1} + 2 = \underline{1.867 \text{ m/s}}. \quad v(-4, 0) = \underline{0}.$$

$$u(0, 4) = \frac{1}{1+4^2} - \frac{-1}{1+4^2} + 2 = \underline{2.118 \text{ m/s}}. \quad v(0, 4) = \frac{4}{1+4^2} - \frac{4}{1+4^2} = \underline{0}.$$

$$8.82 \quad f = \frac{2p}{2p} \ln[x^2 + (y-1)^2]^{1/2} + \frac{2p}{2p} \ln[x^2 + (y+1)^2]^{1/2} = \frac{1}{2} \ln[x^2 + (y-1)^2] + \frac{1}{2} \ln[x^2 + (y+1)^2].$$

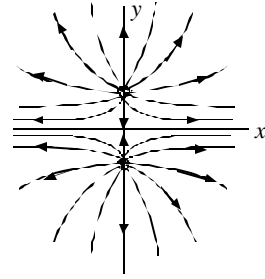
$$u = \frac{\partial f}{\partial x} = \frac{x}{x^2 + (y-1)^2} + \frac{x}{x^2 + (y+1)^2}.$$

$$v = \frac{\partial f}{\partial y} = \frac{y-1}{x^2 + (y-1)^2} + \frac{y+1}{x^2 + (y+1)^2}.$$

At (0, 0) $u = 0$ and $v = 0$. At (1, 1)

$$v = 0 + \frac{2}{2^2 + 1^2} = \frac{2}{5} = 0.4 \text{ m/s. } u = \frac{1}{1^2} + \frac{1}{2^2 + 1^2} = 1.2 \text{ m/s.}$$

$$\therefore \underline{\underline{\vec{V} = 1.2\hat{i} + 0.4\hat{j} \text{ m/s.}}}$$



8.83 $f = \frac{2p}{2p} \ln[(y-1)^2 + x^2]^{1/2} + \frac{2p}{2p} \ln[(y+1)^2 + x^2]^{1/2} + U_\infty x.$

$$= \frac{1}{2} \ln[(y-1)^2 + x^2] + \frac{1}{2} \ln[(y+1)^2 + x^2] + U_\infty x.$$

a) Stag. pts. May occur on x -axis, $y=0$.

$$u = \left. \frac{\partial f}{\partial x} \right|_{y=0} = \frac{x}{1+x^2} + \frac{x}{1+x^2} + 10.$$

$$\therefore x^2 + 0.2x + 1 = 0. \quad \therefore \text{no stagnation points exist on the } x\text{-axis.}$$

(They do exist away from the x -axis.)

Along the y -axis: $u(y) = 10. \quad q = \int_0^h u dy = \frac{1}{2}(2p) = p \text{ m}^2/\text{s}.$

$$\therefore p = \int_0^h 10 dy = 10 h. \quad \therefore h = \underline{\underline{0.314 \text{ m.}}}$$

b) $u = \frac{2x}{1+x^2} + 1. \quad \therefore x^2 + 2x + 1 = 0. \quad \therefore x = -1 \text{ m.}$

Stag. pt.: $(-1, 0)$

Along the y -axis: $u = 1.0. \quad \therefore p = 1 \times h. \quad \therefore h = \underline{\underline{3.14 \text{ m.}}}$

c) $u = \frac{2x}{1+x^2} + 0.2. \quad \therefore x^2 + 10x + 1 = 0. \quad \therefore x = -9.90, -0.10 \text{ m.}$

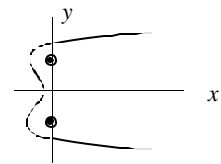
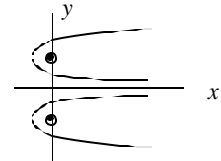
Stag. pts.: $(-9.9, 0), (-0.1, 0).$

Along the y -axis: $u = 0.2. \quad \therefore p = 0.2 h. \quad \therefore h = \underline{\underline{15.71 \text{ m.}}}$

8.84 $f = \frac{60}{r} \cos q + 8r \cos q.$

a) $v_r = \frac{\partial f}{\partial r} = -\frac{60}{r^2} \cos q + 8 \cos q = \left(8 - \frac{60}{r^2}\right) \cos q.$

At the cylinder surface $v_r = 0$ for all q . Hence,



$$\frac{60}{r_c^2} = 8. \quad \therefore r_c = \underline{2.739 \text{ m}}$$

b) Bernoulli: $\Delta p = r \frac{U_\infty^2}{2} = 1000 \frac{8^2}{2} = 32\,000 \text{ Pa}$ or 32 kPa

c) $v_q = \frac{1}{r} \frac{\partial \psi}{\partial q} = -\frac{60}{r^2} \sin q - 8 \sin q$.

At $r = r_c$, $v_q = -8 \sin q - 8 \sin q = \underline{-16 \sin q}$

d) $\Delta p = r \frac{v_{90^\circ}^2}{2} = 1000 \frac{16^2}{2} = 128\,000 \text{ Pa}$ or 128 kPa

8.85 $y = \frac{4p}{2p} q + \frac{20p}{2p} \ln r = 2q + 10 \ln r$

At $(x, y) = (0, 1)$, $(r, q) = (1, p/2)$.

$$v_r(1, p/2) = \frac{1}{r} \frac{\partial \psi}{\partial r} = \frac{1}{1} (2) = 2.$$

$$v_q(1, p/2) = -\frac{\partial \psi}{\partial q} = -\frac{10}{1} = -10.$$

$$v_r(1.7, p/4) = \frac{2}{1.7} = 1.18, \quad v_q(1.7, p/4) = \frac{-10}{1.7} = -5.88$$

$$v_r(3.2, 0) = \frac{2}{3.2} = 0.625, \quad v_q(3.2, 0) = \frac{-10}{3.2} = 3.125$$

$$v_r(6, -p/4) = \frac{2}{6} = 0.333, \quad v_q(6, -p/4) = \frac{-10}{6} = -1.67, \text{ etc.}$$

Note: We scaled the radius at each 45° increment to find r .

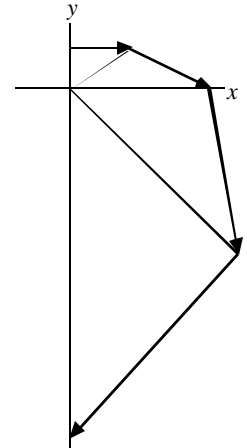
b) $v_r = \frac{2}{r}$ and $v_q = -\frac{10}{r}$. From Table 5.1 (use the l.h.s. of momentum)

$$a_r = \frac{Dv_r}{Dt} + \frac{v_q^2}{r} = v_r \frac{\partial v_r}{\partial r} - \frac{v_q^2}{r} = \frac{2}{r} \left(-\frac{2}{r^2} \right) - \frac{100}{r^3} = -\frac{104}{r^3}$$

$$= -104 \text{ m/s}^2$$

$$a_q = \frac{Dv_q}{Dt} + \frac{v_r v_q}{r} = v_r \frac{\partial v_q}{\partial r} + \frac{v_r v_q}{r} = \frac{2}{r} \left(\frac{10}{r^2} \right) + \frac{2(-10)}{r^3} = 0.$$

$$\therefore \bar{a}(0, 1) = \underline{(-104, 0) \text{ m/s}^2}$$



c) $v_r(14.14, p/4) = 2/14.14 = 0.1414$, $v_q(14.14, p/4) = -\frac{10}{14.14} = -0.707$
 $v_r(0.1, p/2) = 2/0.1 = 20$, $v_q(0.1, p/2) = -10/0.1 = -100$.
 Bernoulli: $\frac{20\,000}{1.2} + \frac{0.1414^2 + 0.707^2}{2} = \frac{p}{1.2} + \frac{20^2 + 100^2}{2}$. $\therefore p = 13\,760\text{ Pa}$
 We used $r_{\text{air}} = 1.2\text{ kg/m}^3$ at standard conditions.

8.86 Along the y-axis $v_r = 0$ and $v_q = -10 - \frac{40}{r^2}$.

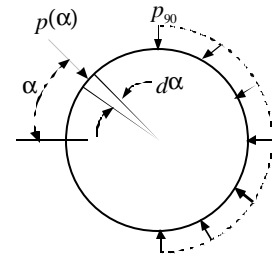
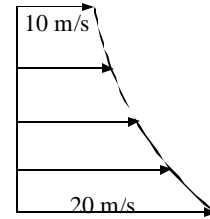
We have set $q = \frac{p}{2}$ in Eq. 8.5.27. $r_c = \sqrt{\frac{40}{10}} = 2$.

b) $v_r = 10 \cos q - \frac{40}{r^2} \cos q$. $(-4, 3) \Rightarrow (5, 126.9^\circ)$.

$v_q = -10 \sin q - \frac{40}{r^2} \sin q$. $\therefore v_r = -6.96\text{ m/s}$, $v_q = -9.28\text{ m/s}$.

c) Use Eq. 8.5.28: $p = p_0 - 2rU_\infty^2 \sin^2 a$

$$\begin{aligned} \text{Drag} &= \int_{-p/2}^{p/2} p \cos a r_c da L - p_{90} \times 2r_c L. \quad p_{90} = p_0 - 2rU_\infty^2. \\ &= 2 \int_0^{p/2} (p_0 - 2rU_\infty^2 \sin^2 a) \cos a r_c L da - p_{90} \times 2r_c L \\ &= 2r_c L \left[p_0 \sin a - 2rU_\infty^2 \frac{\sin^3 a}{3} \right]_0^{p/2} - [p_0 - 2rU_\infty^2] 2r_c L = \frac{8}{3} r_c L r U_\infty^2. \\ C_D &= \frac{\text{Drag}}{\frac{1}{2} r U_\infty^2 A} = \frac{(8/3) r_c L r U_\infty^2}{\frac{1}{2} r U_\infty^2 2r_c L} = \frac{8}{3} = 2.667. \end{aligned}$$



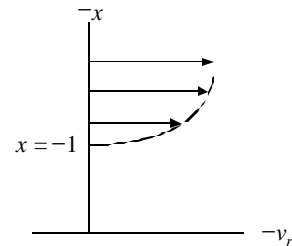
8.87 $v_r = U_\infty \cos q - \frac{m}{r^2} \cos q$. Let $U_\infty = 4$, $m = r_c^2 U_\infty = 1^2 \times 4 = 4$.

For $q = p$, $v_r = -4 + \frac{4}{r^2}$.

b) $v_q = -\frac{m \sin q}{r} = -U_\infty \sin q - \frac{m \sin q}{r_c^2} = \left(-4 - \frac{4}{1^2}\right) \sin q = -8 \sin q$.

c) $p_c = p_\infty + r \frac{V_\infty^2}{2} - r \frac{v_q^2}{2} = 50\,000 + 1000 \times \frac{4^2}{2} - 1000 \frac{8^2 \sin^2 q}{2}$.

$\therefore p_c = 58 - 32 \sin^2 q\text{ kPa}$.



$$\begin{aligned} \text{d) Drag} &= 2 \int_0^{p/2} (58 - 32 \sin^2 \mathbf{a}) \cos \mathbf{a} \times 1 \times 1 d\mathbf{a} - 26 \times 2 \times 1 \\ &= 2 \left[58 - 32 \left(\frac{1}{3} \right) \right] - 52 = \underline{42.7 \text{ kN}}. \quad (\text{See the figure in Problem 8.86c.}) \end{aligned}$$

8.88 On the cylinder $v_q = -2U_\infty \sin \mathbf{q} - \frac{\Gamma}{2pr_c} = -60 \sin \mathbf{q} - \frac{1000}{2p \times 3.651}$, where we have

$$\text{Used } r_c = \sqrt{\frac{m}{U_\infty}} = \sqrt{\frac{400}{30}} = 3.651 \text{ ft.}$$

If

$$u(x, y) = -0.0318 \left[\frac{x-6}{(x-6)^2 + (y-2)^2} + \frac{x-6}{(x-6)^2 + (y+2)^2} + \frac{x+6}{(x+6)^2 + (y-2)^2} + \frac{x+6}{(x+6)^2 + (y+2)^2} \right]$$

$$\therefore \mathbf{q} = 227^\circ, 313^\circ.$$

Stag. pts.: $(3.651 \text{ ft}, 227^\circ)$, $(3.651 \text{ ft}, 313^\circ)$.

Max. pressure occurs on the cylinder at a stagnation pt.:

$$\therefore p_{\max} = \frac{\mathbf{r}}{2} [U_\infty^2 - v_o^2] = \frac{0.0024}{2} [30^2 - 0^2] = \underline{1.08 \text{ psf.}}$$

Min. pressure occurs at the top of the cylinder where $\mathbf{q} = 90^\circ$ and the velocity is:

$$v_{90} = -2U_\infty \sin \mathbf{q} - \frac{\Gamma}{2pr_o} = -2 \times 30 - \frac{1000}{2p \times 3.651} = 104 \text{ fps}$$

$$\therefore p_{\min} = \frac{\mathbf{r}}{2} [U_\infty^2 - v_o^2] = \frac{0.0024}{2} [30^2 - 104^2] = \underline{-11.8 \text{ psf.}}$$

8.89 $v_q = -2 \times 20 \sin \mathbf{q} - \frac{\Gamma}{2p \times 4}$. For one stag. pt.: $v_q = 0$ at $\mathbf{q} = 270^\circ$:

$$0 = -2 \times 20 \sin 270^\circ - \frac{\Gamma}{2p \times 4}. \quad \therefore \Gamma = 2 \times 20 \times 2p \times 4 = 100.5 \text{ m}^2 / \text{s.}$$

$$\Gamma = 2pr_c^2 \mathbf{w}. \quad \therefore \mathbf{w} = \frac{\Gamma}{2pr_c^2} = \frac{100.5}{2p \times 4^2} = \underline{100 \text{ rad} / \text{s.}} \quad (\text{See Example 8.12.})$$

Min. pressure occurs where $|v_q|$ is max, i.e., $\mathbf{q} = p / 2$. There

$$v_q = -2 \times 20 \times 1 - \frac{100.5}{2p \times 4} = 80 \text{ m} / \text{s.}$$

$$\therefore p_{\min} = p_\infty + \frac{V_\infty^2}{2} \mathbf{r} - \frac{v_q^2}{2} \mathbf{r} = 0 + \frac{20^2}{2} \times 1.22 - \frac{80^2}{2} \times 1.22 = \underline{-3660 \text{ Pa.}}$$

8.90 $\Gamma = 2\pi r_c^2 w = 2\pi \times 6^2 \times 120 \times 2\pi / 60 = 28.42 \text{ m}^2 / \text{s}$. $m = r_c^2 U = 6^2 \times 3 = 1.08 \text{ m}^3 / \text{s}$.

$\therefore v_q = -2 \times 3 \sin q - \frac{28.42}{2\pi \times 6}$. $\therefore \sin q = -1.256$. Impossible. \therefore Stag. pt. is off the

cylinder at $q = 270^\circ$, but $r > r_c$. From Eq. 8.5.29,

$$v_q = -\frac{\Gamma y}{\pi r^2} = -U_\infty \sin q - \frac{m}{r^2} \sin q - \frac{\Gamma}{2\pi r} = -3(-1) - \frac{1.08}{r^2}(-1) - \frac{28.42}{2\pi r} = 0.$$

$\therefore 3 + \frac{1.08}{r^2} = \frac{4.523}{r}$. $\therefore r^2 - 1.508r + 0.36 = 0$. $\therefore r = 1.21 \text{ m}$.

Stag. pt.: (1.21, 270°). $(v_q)_{90^\circ} = -2 \times 3 - \frac{28.42}{2\pi \times 6} = -1354 \text{ m/s}$.

Min. pressure occurs at $q = 90^\circ$, at $r = r_c$: $p_{\min} = \left(\frac{3^2}{2} - \frac{13.54^2}{2} \right) 1.22 = \underline{-106 \text{ Pa}}$.

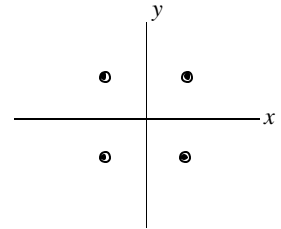
Max. pressure occurs at $q = 270^\circ$, at $r = r_c$: $p_{\max} = \left(\frac{3^2}{2} - \frac{1.54^2}{2} \right) 1.22 = \underline{-4.04 \text{ Pa}}$.

8.91 At 15,000 ft, $r = .0015 \text{ slug} / \text{ft}^3$.

Lift = $rU_\infty \Gamma L = .0015 \times 350 \times 15,000 \times 60 = \underline{472,000 \text{ lb}}$.

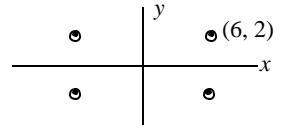
8.92 Place four sources as shown. Then, with $q = 2\pi$ for each:

$$u(x,y) = \frac{x-2}{(x-2)^2 + (y-2)^2} + \frac{x+2}{(x+2)^2 + (y-2)^2} + \frac{x-2}{(x-2)^2 + (y+2)^2} + \frac{x+2}{(x+2)^2 + (y+2)^2}$$



$$v(x,y) = \frac{y-2}{(x-2)^2 + (y-2)^2} + \frac{y+2}{(x-2)^2 + (y+2)^2} + \frac{y-2}{(x+2)^2 + (y-2)^2} + \frac{y+2}{(x+2)^2 + (y+2)^2}$$

8.93 Place four sources with $q = 0.2 \text{ m}^2 / \text{s}$, as shown.



$$u(x,y) = -.0318 \left[\frac{x-6}{(x-6)^2 + (y-2)^2} + \frac{x-6}{(x-6)^2 + (y+2)^2} + \frac{x+6}{(x+6)^2 + (y-2)^2} + \frac{x+6}{(x+6)^2 + (y+2)^2} \right]$$

$$v(x,y) = -.0318 \left[\frac{y-2}{(x-6)^2 + (y-2)^2} + \frac{y-2}{(x+6)^2 + (y-2)^2} + \frac{y+2}{(x-6)^2 + (y+2)^2} + \frac{y+2}{(x+6)^2 + (y+2)^2} \right]$$

where $\frac{q}{2\pi} = \frac{-.2}{2\pi} = -.0318$.

$$\text{At } (4,3) \quad u(4,3) = -0.0318 \left[\frac{-2}{4+1} + \frac{-2}{4+25} + \frac{10}{100+1} + \frac{10}{100+25} \right] = \underline{0.00922 \text{ m/s.}}$$

$$v(4,3) = -0.0318 \left[\frac{1}{4+1} + \frac{1}{100+1} + \frac{5}{4+25} + \frac{5}{100+25} \right] = \underline{-0.01343 \text{ m/s.}}$$

8.94 $\text{Re}_{\text{crit}} = \frac{U_{\infty} x_T}{\nu}$. $\therefore x_T = 6 \times 10^5 \nu / 300 = 2000\nu$.

a) $\nu = 1.56 \times 10^{-4} \text{ ft}^2 / \text{sec}$. $\therefore x_T = 2000 \times 1.56 \times 10^{-4} = 0.312'$ or 3.74"

b) $\nu = \frac{\mu}{\rho} = 2.1 \times 10^{-4} \text{ ft}^2 / \text{sec}$. $\therefore x_T = 2000 \times 2.1 \times 10^{-4} = 0.42'$ or 5.04"

c) $\nu = 3.47 \times 10^{-4} \text{ ft}^2 / \text{sec}$. $\therefore x_T = 2000 \times 3.47 \times 10^{-4} = 0.694'$ or 8.33"

8.95 a) Use $\text{Re}_{\text{crit}} = 3 \times 10^5 = 10x_T / 1.51 \times 10^{-5}$. $\therefore x_T = \underline{0.453 \text{ m}}$.

b) Use $\text{Re}_{\text{crit}} = 10^6 = 10x_T / 1.51 \times 10^{-5}$. $\therefore x_T = \underline{1.51 \text{ m}}$.

c) Use $\text{Re}_{\text{crit}} = 3 \times 10^5 = 10x_T / 1.51 \times 10^{-5}$. $\therefore x_T = \underline{0.453 \text{ m}}$.

d) Use $\text{Re}_{\text{crit}} = 3 \times 10^5 = 10x_T / 1.51 \times 10^{-5}$. $\therefore x_T = \underline{0.453 \text{ m}}$.

e) $\text{Re} = 6 \times 10^4 = 10x_{\text{growth}} / 1.51 \times 10^{-5}$. $\therefore x_{\text{growth}} = 0.091 \text{ m}$ or 9.1 cm.

Note: A rough plate, high free-stream disturbances, or a vibrated smooth plate all experience transition at the lower Re_{crit} .

8.96 a) Use $\text{Re}_{\text{crit}} = 3 \times 10^5 = 10x_T / 10^{-6}$. $\therefore x_T = 0.03 \text{ m}$ or 3 cm.

b) Use $\text{Re}_{\text{crit}} = 10^6 = 10x_T / 10^{-6}$. $\therefore x_T = 0.1 \text{ m}$ or 10 cm.

c) Use $\text{Re}_{\text{crit}} = 3 \times 10^5 = 10x_T / 10^{-6}$. $\therefore x_T = 0.03 \text{ m}$ or 3 cm.

d) Use $\text{Re}_{\text{crit}} = 3 \times 10^5 = 10x_T / 10^{-6}$. $\therefore x_T = 0.03 \text{ m}$ or 3 cm.

e) $p(x) = 20\,000 - 2 \times 1000 \times 10^2 \sin^2(x/2)$

8.97 $\text{Re}_{\text{crit}} = 6 \times 10^5 = \frac{U_{\infty} \times 2}{\nu}$. For a wind tunnel: $6 \times 10^5 = \frac{U_{\infty} \times 2}{1.5 \times 10^{-5}}$.
 $\therefore \underline{U_{\infty} = 4.5 \text{ m/s}}$.

For a water channel: $6 \times 10^5 = \frac{U_{\infty} \times 2}{10^{-6}}$. $\therefore \underline{U_{\infty} = 0.3 \text{ m/s}}$.

8.98 The x -coordinate is measured along the cylinder surface as shown in Fig. 8.19. The pressure distribution (see solution 8.86) on the surface is $p = p_0 - 2rU_{\infty}^2 \sin^2 \alpha$ where $r\alpha = x$ (α is zero at the stagnation point). Then

$$p(x) = 20\,000 - 2 \times 1000 \times 10^2 \sin^2(x/2)$$

$$= \underline{20 - 200 \sin^2(x/2) \text{ kPa}}$$

The velocity $U(x)$ at the edge of the b.l. is $U(x)$ on the cylinder wall:

$$v_q(r=2) = -10 \sin q - 10 \sin q = -20 \sin(p - a) = 20 \sin a$$

$$\therefore U(x) = \underline{20 \sin(x/2)}$$

8.99 $U(x) = v_q$ at $r_c = 1$. $v_q = 8 \sin a$. $\therefore U(x) = \underline{8 \sin x}$ since $x = a r_c$.

$$p(x) = 58 - 32 \sin^2 a = \underline{58 - 32 \sin^2 x \text{ kPa}}$$

8.100 The height h above the plate is $h(x) = mx + 4$. $1 = m \times 2 + 4 \therefore m = -15$

$$\therefore h(x) = 0.4 - 15x$$
 Continuity: $6 \times 4 = U(x)h$. $\therefore U(x) = \frac{2.4}{0.4 - 15x}$ or

$$U(x) = \frac{16}{2.67 - x}$$

Euler's Eqn: $ru \frac{du}{dx} = -\frac{rp}{r} \therefore \frac{dp}{dx} = r \frac{16}{2.67 - x} \frac{16}{(2.67 - x)^2}$

$$= \frac{256}{(2.67 - x)^3}$$

8.101 a) $\dot{m}_{\text{top}} = \dot{m}_{\text{out}} - \dot{m}_{\text{in}} = \int_0^d r u dy + \frac{\partial}{\partial x} \int_0^d r u dy dx - \int_0^d r u dy = \frac{\partial}{\partial x} \int_0^d r u dy dx$

b) $\Sigma F_x = p d - t_0 dx + (p + \frac{dp}{2}) dd - (p + dp)(d + dd)$

$$= -t_0 dx - d dp + \text{higher order terms}$$

$$\dot{m}_{\text{out}} - \dot{m}_{\text{in}} - \dot{m}_{\text{top}} = \int_0^d r u^2 dy + \frac{\partial}{\partial x} \int_0^d r u^2 dy dx - \int_0^d r u^2 dy - U(x) \left(\frac{\partial}{\partial x} \int_0^d r u dy dx \right)$$

$$= \frac{\partial}{\partial x} \int_0^d r u^2 dy dx - U(x) \left(\frac{\partial}{\partial x} \int_0^d r u dy dx \right)$$

$$= 4 \left[-\frac{3 \times 4}{2 \times 4.65^2 \times 1.5 \times 10^{-5} \times 3} y + \frac{3}{2} \frac{4^2 y^3}{4.65^4 \times (1.5 \times 10^{-5} \times 3)^2} \right] \frac{dd}{dx}$$

8.102 $t_0 = -d \frac{dp}{dx} + U(x) \frac{d}{dx} \int_0^d r u dy - \frac{d}{dx} \int_0^d r u^2 dy$

$$= -d \frac{dp}{dx} + \frac{d}{dx} \int_0^d r u U dy - \frac{dU}{dx} \left(\int_0^d r u dy \right) - \frac{d}{dx} \int_0^d r u^2 dy$$

where we have used $g \frac{df}{dx} = \frac{dfg}{dx} - f \frac{dg}{dx}$. (Here $U = g$, $f = \int_0^d r u dy$.)

$$\therefore t_0 = -d \frac{dp}{dx} + \frac{d}{dx} \int_0^d r u (U - u) dy - r \frac{dU}{dx} \int_0^d u dy. \quad (r = \text{const.})$$

$$8.103 \quad \frac{dp}{dx} = -\frac{r}{2} \frac{d}{dx} U^2 = -rU \frac{dU}{dx} = -r \frac{dU}{dx} \left(\frac{1}{d} \int_0^d U dy \right) \text{ where } U = \frac{1}{d} \int_0^d U dy.$$

$$\begin{aligned} \therefore t_0 &= -d \left[-r \frac{dU}{dx} \left(\frac{1}{d} \int_0^d U dy \right) \right] + r \frac{d}{dx} (qU^2) - r \frac{dU}{dx} \int_0^d u dy \\ &= r \frac{d}{dx} (qU^2) + r \frac{dU}{dx} \int_0^d (U - u) dy = r \frac{d}{dx} (qU^2) + r \frac{dU}{dx} U d. \end{aligned}$$

$$8.104 \quad \text{If } dp/dx = 0 \text{ then } \frac{dU}{dx} = 0 \text{ and } t_0 = r \frac{d}{dx} \int_0^d u(U_\infty - u) dy.$$

$$t_0 = r \frac{d}{dx} \int_0^d U_\infty^2 \sin \frac{py}{2d} \left(1 - \sin \frac{py}{2d} \right) dy = r U_\infty^2 \frac{d}{dx} \left[-\frac{2d}{p} \cos \frac{py}{2d} - \frac{y}{2} \right]_0^d = r U_\infty^2 \frac{d}{dx} \left(\frac{2d}{p} - \frac{d}{2} \right)$$

$$t_0 = m \frac{\int u}{\int y} \Big|_{y=0} = m U_\infty \frac{p}{2d} \cos 0.$$

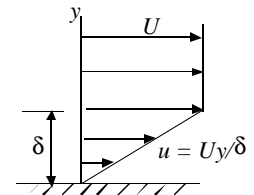
$$\therefore m U_\infty \frac{p}{2d} = .137 r U_\infty^2 \frac{dd}{dx}. \quad \therefore ddd = 11.5 \frac{n}{U_\infty} dx. \quad \therefore d = 4.79 \sqrt{\frac{nx}{U_\infty}}.$$

$$b) \quad t_0 = m U_\infty \frac{p}{2} \frac{1}{4.79} \sqrt{\frac{U_\infty}{nx}} = 0.328 m U_\infty \sqrt{\frac{U_\infty}{nx}}.$$

$$c) \quad \frac{\int u}{\int x} = U_\infty \frac{\int \sin \left(\frac{py}{2 \times 4.79} \sqrt{\frac{U_\infty}{nx}} \right)}{\int x} = U_\infty \frac{\int \sin \left(\frac{a}{\sqrt{x}} \right)}{\int x} = U_\infty \left(-\frac{ax^{-3/2}}{2} \right) \cos \frac{a}{\sqrt{x}} = -\frac{\int v}{\int y}.$$

$$\therefore v = \int_0^d U_\infty \frac{.164y}{x^{3/2}} \sqrt{\frac{U_\infty}{n}} \cos \left(.328y \sqrt{\frac{U_\infty}{nx}} \right) dy = \int_0^d .0316 U_\infty \sqrt{\frac{U_\infty}{n}} \cos \left[\left(.189 \sqrt{\frac{U_\infty}{n}} \right) y \right] dy.$$

$$8.105 \quad u = U_\infty \frac{y}{d}. \quad t_0 = r \frac{d}{dx} \int_0^d U_\infty^2 \frac{y}{d} \left(1 - \frac{y}{d} \right) dy \\ = r \frac{d}{dx} U_\infty^2 \left(\frac{d}{2} - \frac{d}{3} \right) = \frac{1}{6} r U_\infty^2 \frac{dd}{dx}.$$



$$t_0 = m \frac{\int u}{\int y} = m \frac{U_\infty}{d}. \quad \therefore m \frac{U_\infty}{d} = \frac{1}{6} r U_\infty^2 \frac{dd}{dx}. \quad \therefore ddd = 6 \frac{n}{U_\infty} dx$$

$$\therefore d^2 = 12 \frac{n}{U_\infty} x. \quad d(x) = 3.46 \sqrt{\frac{nx}{U_\infty}}. \quad t_0 = 0.289 m U_\infty \sqrt{\frac{U_\infty}{nx}}.$$

$$\% \text{error in } d(x) = \frac{5 - 3.46}{5} \times 100 = \underline{30.8\% \text{ low.}}$$

$$\% \text{error in } t_0(x) = \frac{.332 - .289}{.332} \times 100 = \underline{13\% \text{ low.}}$$

$$\begin{aligned} 8.106 \quad t_0 &= \frac{d}{dx} \left\{ \int_0^{d/6} r 3U_\infty^2 \frac{y}{d} \left(1 - 3\frac{y}{d} \right) dy + \int_{d/6}^{d/2} r U_\infty^2 \left(\frac{y}{d} + \frac{1}{3} \right) \left(1 - \frac{y}{d} - \frac{1}{3} \right) dy \right. \\ &\quad \left. + \int_{d/2}^d r U_\infty^2 \left(\frac{y}{3d} + \frac{2}{3} \right) \left(1 - \frac{y}{3d} - \frac{2}{3} \right) dy \right\} \\ &= \frac{d}{dx} r U_\infty^2 (0.1358d) = m \frac{3U_\infty}{d}. \quad \therefore d \frac{dd}{dx} = 22.08 m / r U_\infty. \end{aligned}$$

$$\text{Thus, } d(x) = 6.65 \sqrt{vx / U_\infty}, \quad t_0(x) = 0.1358 r U_\infty^2 \left(\frac{6.65}{2} \sqrt{\frac{v}{U_\infty x}} \right) = \underline{0.451 r U_\infty^2 \text{Re}_x^{-1/2}}.$$

$$\% \text{error for } d = \frac{6.65 - 5}{5} \times 100 = \underline{33\%}, \quad \% \text{error for } t_0 = \frac{0.451 - 0.332}{0.332} \times 100 = \underline{36\%}$$

$$8.107 \quad \text{Continuity from entrance to } x: \quad U_0 H = 2 \int_0^d u(y) dy + U(x)(H - 2d).$$

$$\text{Write } U(x)d = U(x) \int_0^d dy = \int_0^d U(x) dy. \quad \text{Then, continuity provides}$$

$$\begin{aligned} U_0 H &= 2 \int_0^d (u - U) dy + UH = UH - 2 \int_0^d (U - u) dy \\ &= UH - 2Ud_d. \quad \therefore U(x) = \frac{U_0 H}{H - 2d_d}. \end{aligned}$$

If we were to move the walls out a distance $d_d(x)$, then $U(x)$ would be constant since $[(H - 2d_d) + 2d_d]$ would be constant; then $U(x) = U_0$. For a square wind tunnel, displace one wall outward $4d_d$ for $dp / dx = 0$.

8.108 The given velocity profile is that used in Example 8.13. There we found $d = 5.48 \sqrt{nx / U_\infty} = 5.48 \sqrt{10^{-6} x / 10} = 0.00173 \sqrt{x} = 0.00173 \sqrt{3} = 0.003 \text{ m}$. Assume the streamline is outside the b.l. Continuity is then

$$\begin{aligned} 10 \times 0.02 &= \int_0^{.003} 10 \left(\frac{2y}{.003} - \frac{y^2}{.003^2} \right) dy + (h - .003)10 \\ &= 0.02 + 10h - 0.03. \quad \therefore h = 0.021 \text{ m or } \underline{2.1 \text{ cm}} \end{aligned}$$

$$d_d = \frac{1}{10} \int_0^{.003} \left(10 - \frac{20y}{.003} + \frac{10y^2}{.003^2} \right) dy = \frac{1}{10} [.03 - .03 + .01] = \underline{0.001 \text{ m}}$$

$$h - 2 = 2.1 - 2 = 0.1 \text{ cm or } 0.001 \text{ m.}$$

The streamline moves away from the wall a distance d_d .

8.109 From Prob. 8.107 we found that we should displace the one wall outward $4d_d$.
From the definition of d_d :

$$h(x) = 4d_d = \frac{4}{10} \int_0^d \left(10 - \frac{20y}{d} + \frac{10y^2}{d^2} \right) dy = 4 \left(d - d + \frac{d}{3} \right) = \frac{4}{3} d$$

$$= \frac{4}{3} \left(5.48 \sqrt{\frac{1.86 \times 10^{-5} x / 10}{160 / (.287 \times 303)}} \right) = \underline{0.00735 \sqrt{x} \text{ m}}$$

We used $d(x)$ found in Example 8.13, $r = p / RT$, and $n = m / r$.

8.110 a) $u = U_\infty \left(\frac{3y}{2d} - \frac{1y^3}{2d^3} \right)$. $d_d = \frac{1}{U_\infty} \int_0^d U_\infty \left(1 - \frac{3y}{2d} + \frac{1y^3}{2d^3} \right) dy = d - \frac{3}{4}d + \frac{1}{8}d = .375d$.

From Eq. 8.6.16, $d_d = .375 \times 4.65 \sqrt{\frac{nx}{U_\infty}} = 1.74 \sqrt{\frac{nx}{U_\infty}}$. %error = 1.2%.

$$q = \frac{1}{U_\infty^2} \int_0^d U_\infty^2 \left(\frac{3y}{2d} - \frac{1y^3}{2d^3} \right) \left(1 - \frac{3y}{2d} + \frac{1y^3}{2d^3} \right) dy = 0.139d$$

$\therefore q = .139 \times 4.65 \sqrt{\frac{nx}{U_\infty}} = 0.648 \sqrt{\frac{nx}{U_\infty}}$. %error = $\frac{.648 - .644}{.644} \times 100 = \underline{0.62\%}$

b) $u = U_\infty \left(2\frac{y}{d} - \frac{y^2}{d^2} \right)$. See Example 8.13. $d_d = \int_0^d \left(1 - \frac{2y}{d} + \frac{y^2}{d^2} \right) dy = d - d + \frac{d}{3} = d / 3$.

$\therefore d_d = \frac{5.48}{3} \sqrt{\frac{nx}{U_\infty}} = 1.83 \sqrt{\frac{nx}{U_\infty}}$. %error = $\frac{1.83 - 1.72}{1.72} \times 100 = \underline{6.4\%}$.

$$q = \int_0^d \left(2\frac{y}{d} - \frac{y^2}{d^2} \right) \left(1 - 2\frac{y}{d} + \frac{y^2}{d^2} \right) dy = d - \frac{1}{3}d - \frac{4}{3}d + \frac{2}{4}d + \frac{2}{4}d - \frac{1}{5}d = .1333d$$

$\therefore q = .1333 \times 5.48 \sqrt{\frac{nx}{U_\infty}} = 0.731 \sqrt{\frac{nx}{U_\infty}}$. %error = $\frac{.731 - .644}{.644} \times 100 = \underline{13.5\%}$.

c) $d_d = \int_0^d \left(1 - \sin \frac{py}{2d} \right) dy = d - \frac{2d}{p} = 0.363d$. See Problem 8.104. $d = 4.79 \sqrt{\frac{nx}{U_\infty}}$.

$\therefore d_d = 0.363 \times 4.79 \sqrt{\frac{nx}{U_\infty}} = 1.74 \sqrt{\frac{nx}{U_\infty}}$. %error = $\frac{1.74 - 1.72}{1.72} \times 100 = \underline{1.2\%}$

$$q = \int_0^d \sin \frac{py}{2d} \left(1 - \sin \frac{py}{2d} \right) dy = \left[-\frac{2d}{p} \cos \frac{py}{2d} - \frac{y}{2} + \sin \text{- term} \right]_0^d = -\frac{d}{2} + \frac{2d}{p} = 0.137d$$

$\therefore q = .137 \times 4.79 \sqrt{\frac{nx}{U_\infty}} = 0.654 \sqrt{\frac{nx}{U_\infty}}$. %error = $\frac{.654 - .644}{.644} \times 100 = \underline{1.6\%}$.

$$8.111 \text{ a) } d = 4.65 \sqrt{\frac{nx}{U_\infty}} = 4.65 \left(\frac{1.6 \times 10^{-4} \times 20}{12} \right)^{1/2} = \underline{0.0759 \text{ ft.}}$$

$$\text{b) } t_0 = .323 r U_\infty^2 \sqrt{\frac{n}{x U_\infty}} = .323 \times .0024 \times 12^2 \left(\frac{1.6 \times 10^{-4}}{20 \times 12} \right)^{1/2} = \underline{9.11 \times 10^{-5} \text{ psf.}}$$

$$\begin{aligned} \text{c) Drag} &= \frac{1}{2} r U_\infty^2 \times 20 \times 15 \times 1.29 \sqrt{\frac{n}{L U_\infty}} \\ &= \frac{1}{2} \times .0024 \times 12^2 \times 300 \times 1.29 \left(\frac{1.6 \times 10^{-4}}{20 \times 12} \right)^{1/2} = \underline{0.0546 \text{ lb.}} \end{aligned}$$

$$\begin{aligned} \text{d) } d_{x=10} &= 4.65 \sqrt{\frac{1.6 \times 10^{-4} \times 10}{12}} = 0.0416 \text{ ft.} \quad \frac{f_u}{f_x} = U_\infty \left[-\frac{3y}{2d^2} + \frac{3y^3}{2d^4} \right] \frac{dd}{dx} \\ \therefore \frac{f_u}{f_x} &= 12 \left[-\frac{3y}{.2 \times .0416^2} + \frac{3y^3}{.2 \times .0416^4} \right] \frac{4.65}{2} \sqrt{\frac{1.6 \times 10^{-4}}{10 \times 12}} = -27.9y + 16140y^3 \\ \therefore v &= \int_0^d -\frac{f_u}{f_x} dy = \frac{27.9}{2} \times .0416^2 - \frac{16140}{4} \times .0416^4 = \underline{0.0121 \text{ fps.}} \end{aligned}$$

$$8.112 \text{ a) } d = 4.65 \sqrt{\frac{nx}{U_\infty}} = 4.65 \left(\frac{15 \times 10^{-5} \times 6}{4} \right)^{1/2} = \underline{0.0221 \text{ m.}}$$

$$\text{b) } t_0 = 0.323 r U_\infty^2 \sqrt{\frac{n}{x U_\infty}} = .323 \times 1.22 \times 4^2 \left(\frac{15 \times 10^{-5}}{6 \times 4} \right)^{1/2} = \underline{0.00498 \text{ Pa.}}$$

$$\text{c) Drag} = \frac{1}{2} r U_\infty^2 L w \times 1.29 \sqrt{\frac{v}{L U_\infty}} = \frac{1}{2} \times 1.22 \times 4^2 \times 6 \times 5 \times 1.29 \left(\frac{15 \times 10^{-5}}{6 \times 4} \right)^{1/2} = \underline{0.299 \text{ N.}}$$

$$\begin{aligned} \text{d) } \frac{f_u}{f_x} &= U_\infty \left[-\frac{3y}{2d^2} + \frac{3y^3}{2d^4} \right] \frac{dd}{dx} \\ &= 4 \left[-\frac{3 \times 4}{2 \times 4.65^2 \times 1.5 \times 10^{-5} \times 3} y + \frac{3}{2} \frac{4^2 y^3}{4.65^4 \times (1.5 \times 10^{-5} \times 3)^2} \right] \frac{dd}{dx} \\ \therefore \frac{f_u}{f_x} &= 4 \left[-6166y + 2.53 \times 10^7 y^3 \right] \frac{4.65}{2} \sqrt{\frac{15 \times 10^{-5}}{4}} \frac{1}{\sqrt{3}} = -64.1y + 2.63 \times 10^5 y^3 \\ \therefore v &= \int_0^d -\frac{f_u}{f_x} dy = \frac{64.1}{2} \times .0156^2 - \frac{2.63 \times 10^5}{4} \times .0156^4 = \underline{0.00391 \text{ m/s.}} \end{aligned}$$

$$\text{where } d_{x=3} = 4.65 \sqrt{\frac{15 \times 10^{-5} \times 3}{4}} = .01560 \text{ m.}$$

$$8.113 \text{ a) } d = 5 \sqrt{\frac{nx}{U_\infty}} = 5 \left(\frac{1.5 \times 10^{-5} \times 2}{10} \right)^{1/2} = \underline{0.00866 \text{ m}}. \text{ Use } t_0 = .332 r U_\infty^2 \sqrt{\frac{n}{x U_\infty}}.$$

$$\text{Drag} = \int_0^L t_0 w dx = .332 \times 1.22 \times 10^2 \sqrt{\frac{1.5 \times 10^{-5}}{10}} \frac{\sqrt{2}}{1/2} \times 4 = \underline{0.561 \text{ N}}.$$

$$\text{b) } d = .38 \times 2 \left(\frac{1.5 \times 10^{-5}}{10 \times 2} \right)^{.2} = \underline{0.0453 \text{ m}}.$$

$$\text{Drag} = \frac{1}{2} r U_\infty^2 L w \times .074 \left(\frac{n}{U_\infty L} \right)^{.2} = \frac{1}{2} \times 1.22 \times 10^2 \times 2 \times 4 \times .074 \left(\frac{1.5 \times 10^{-5}}{10 \times 2} \right)^{.2} = \underline{2.15 \text{ N}}.$$

$$8.114 \text{ a) } d = .38 \times 6 \left(\frac{1.5 \times 10^{-5}}{20 \times 6} \right)^{.2} = \underline{0.0949 \text{ m}}. \quad t_0 = \frac{1}{2} \times 1.22 \times 20^2 \times .059 \left(\frac{1.5 \times 10^{-5}}{20 \times 6} \right)^{.2} = \underline{.6 \text{ Pa}}.$$

$$\text{b) } d = .38 \times 6 \left(\frac{10^{-6}}{20 \times 6} \right)^{.2} = \underline{0.0552 \text{ m}}. \quad t_0 = \frac{1}{2} \times 1000 \times 20^2 \times .059 \left(\frac{10^{-6}}{20 \times 6} \right)^{.2} = \underline{286 \text{ Pa}}.$$

$$8.115 \quad u(y=d) = U_\infty. \quad \frac{\partial u}{\partial y} = \frac{1}{7} U_\infty y^{-6/7} d^{-1/7}. \quad \left. \frac{\partial u}{\partial y} \right|_{y=d} = \frac{1}{7} U_\infty / d.$$

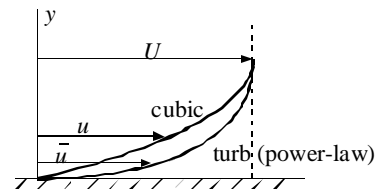
$\left. \frac{\partial u}{\partial y} \right|_{y=d}$ should be zero. Thus, this condition is not satisfied.

$$t_0 = m \left. \frac{\partial u}{\partial y} \right|_{y=0} = m \frac{1}{7} U_\infty \frac{1}{0} d^{-1/7} = \infty. \text{ Thus, this is unacceptable and}$$

$\frac{\partial u}{\partial y}$ at, and near, the wall is not valid.

$$u = U_\infty \left(\frac{3y}{2d} - \frac{1}{2} \frac{y^3}{d^3} \right).$$

$$\bar{u} = U_\infty \left(\frac{y}{d} \right)^{1/7}.$$



$$8.116 \text{ a) Drag} =$$

$$\frac{1}{2} \times .0024 \times 20^2 \times (12 \times 15) \left[.074 \left(\frac{1.58 \times 10^{-4}}{20 \times 12} \right)^{.2} - 1060 \left(\frac{1.58 \times 10^{-4}}{20 \times 12} \right) \right] = \underline{0.31 \text{ lb}}.$$

b) Drag =

$$\frac{1}{2} \times .0024 \times 20^2 \times (12 \times 15) \left[.074 \left(\frac{1.58 \times 10^{-4}}{20 \times 12} \right)^2 - 1700 \left(\frac{1.58 \times 10^{-4}}{20 \times 12} \right) \right] = \underline{0.27 \text{ lb.}}$$

c) Drag =

$$\frac{1}{2} \times .0024 \times 20^2 \times (12 \times 15) \left[.074 \left(\frac{1.58 \times 10^{-4}}{20 \times 12} \right)^2 - 2080 \left(\frac{1.58 \times 10^{-4}}{20 \times 12} \right) \right] = \underline{0.25 \text{ lb.}}$$

$$8.117 \text{ a) Drag} = \frac{1}{2} \times 1000 \times 1.2^2 \times (1 \times 2) \left[.074 \left(\frac{10^{-6}}{1.2 \times 1} \right)^2 - 1060 \left(\frac{10^{-6}}{1.2 \times 1} \right) \right] = \underline{5.21 \text{ N.}}$$

$$\text{b) Drag} = \frac{1}{2} \times 1000 \times 1.2^2 \times (1 \times 2) \left[.074 \left(\frac{10^{-6}}{1.2 \times 1} \right)^2 - 1700 \left(\frac{10^{-6}}{1.2 \times 1} \right) \right] = \underline{4.44 \text{ N.}}$$

$$\text{c) Drag} = \frac{1}{2} \times 1000 \times 1.2^2 \times (1 \times 2) \left[.074 \left(\frac{10^{-6}}{1.2 \times 1} \right)^2 - 2080 \left(\frac{10^{-6}}{1.2 \times 1} \right) \right] = \underline{3.99 \text{ N.}}$$

$$8.118 \quad U_\infty = 60 \frac{1000}{3600} = 16.67 \text{ m/s.} \quad d = .38 \times 100\,000 \left(\frac{1.5 \times 10^{-5}}{16.67 \times 10^5} \right)^2 = \underline{235 \text{ m.}}$$

$$t_0 = \frac{1}{2} r U_\infty^2 c_f = \frac{1}{2} \times 1.22 \times 16.67^2 \times \left[.059 \left(\frac{1.5 \times 10^{-5}}{16.67 \times 10^5} \right)^2 \right] = \underline{0.0618 \text{ Pa.}}$$

$$\text{b) } t_0 = \frac{1}{2} r U_\infty^2 c_f = \frac{1}{2} \times 1.22 \times 16.67^2 \frac{.455}{\left[\ln \left(.06 \frac{16.67 \times 10^5}{1.5 \times 10^{-5}} \right) \right]^2} = \underline{0.151 \text{ Pa.}}$$

$$\therefore u_t = \sqrt{\frac{.151}{1.22}} = .351 \text{ m/s.} \quad \therefore \frac{16.67}{.351} = 2.44 \ln \frac{.351 d}{1.5 \times 10^{-5}} + 7.4. \quad \therefore d = \underline{585 \text{ m.}}$$

Both (a) and (b) are in error, however, (b) is more accurate. $\frac{\eta p}{\eta x} < 0$.

$$8.119 \text{ a) } 5 = \frac{u_t d_n}{n} \quad (\text{See Fig. 8.24 b).} \quad \therefore d_n = \frac{5 \times 1.5 \times 10^{-5}}{.351} = \underline{2.14 \times 10^{-4} \text{ m.}}$$

$$\begin{aligned} \text{b) } d_d &= \frac{1}{U_\infty} \int_0^d (U_\infty - \bar{u}) dy = \frac{m_t}{U_\infty} \int_{d_n}^{.15d} \left(2.5 - 2.44 \ln \frac{y}{d} \right) dy + \frac{u_t}{U_\infty} \int_{.15d}^d -3.74 \ln \frac{y}{d} dy \\ &= \frac{u_t}{U_\infty} \left[2.5(.15d - d_n) - 2.44 \left(y \ln \frac{y}{d} - y \right) \Big|_{d_n}^{.15d=87.8} - 3.74 \left(y \ln \frac{y}{d} - y \right) \Big|_{87.8}^{d=585} \right] \\ &= \frac{.351}{16.67} [219 + 620 - .008 + 2188 - 951] = \underline{43.7 \text{ m.}} \end{aligned}$$

Note: We cannot use zero as a lower limit since the ln-profile does not go to the

wall. Hence, we use d_n ; the lower limit provides a negligible contribution to the integral.

$$8.120 \text{ a) Use Eq. 8.6.40: } c_f = \frac{.455}{\left[\ln\left(.06 \frac{300 \times 20}{1.58 \times 10^{-4}} \right) \right]^2} = \underline{0.00212}.$$

$$\text{b) } t_0 = \frac{1}{2} r U_\infty^2 c_f = \frac{1}{2} \times .0024 \times 300^2 \times .00212 = \underline{0.229 \text{ psf.}} \quad u_t = \sqrt{\frac{.229}{.0024}} = 9.77 \text{ fps.}$$

$$\text{c) } d_n = \frac{5n}{u_t} = 5 \times 1.58 \times 10^{-4} / 9.77 = \underline{8.09 \times 10^{-5} \text{ ft.}}$$

$$\text{d) } \frac{300}{9.77} = 2.44 \ln \frac{9.77 d}{1.58 \times 10^{-4}} + 7.4. \quad \therefore \underline{d = 0.228 \text{ ft.}}$$

$$8.121 \text{ a) } t_0 = \frac{1}{2} r U_\infty^2 c_f = \frac{1}{2} \times 1000 \times 10^2 \frac{.455}{\left[\ln\left(.06 \frac{10 \times 3}{10^{-6}} \right) \right]^2} = 110 \text{ Pa.}$$

$$\therefore u_t = \sqrt{\frac{110}{1000}} = .332 \text{ m/s.} \quad \therefore d_n = \frac{5n}{u_t} = \frac{5 \times 10^{-6}}{.332} = \underline{1.51 \times 10^{-5} \text{ m.}}$$

$$\text{b) } \bar{u} = 5u_t = 5 \times .332 = \underline{1.66 \text{ m/s.}}$$

$$\text{c) } y = .15d. \quad \text{— Do part (d) first!} \quad \therefore y = .15 \times .0333 = \underline{0.005 \text{ m.}}$$

$$\text{d) } \frac{10}{.332} = 2.44 \ln \frac{.332 d}{10^{-6}} + 7.4. \quad \therefore \underline{d = 0.0333 \text{ m.}}$$

$$8.122 \text{ Assume flat plates with } dp/dx = 0. \quad C_f = \frac{.523}{\left[\ln\left(.06 \frac{10 \times 100}{10^{-6}} \right) \right]^2} = .00163.$$

$$\therefore \text{Drag} = 2 \times \frac{1}{2} \times 1000 \times 10^2 \times 10 \times 100 \times .00163 = \underline{163 \text{ 000 N.}}$$

To find d_{\max} we need u_t .

$$t_0 = \frac{1}{2} \times 1000 \times 10^2 \frac{.455}{\left[\ln\left(.06 \frac{10 \times 100}{10^{-6}} \right) \right]^2} = 70.9 \text{ Pa.} \quad \therefore u_t = \sqrt{\frac{70.9}{1000}} = 0.266 \text{ m/s.}$$

$$\frac{10}{.266} = 2.44 \ln \frac{.266 d}{10^{-6}} + 7.4. \quad \therefore \underline{d_{\max} = 0.89 \text{ m.}}$$

$$8.123 \text{ a) Assume a flat plate of width } pD. \quad \text{Re} = \frac{UL}{n} = \frac{15 \times 600}{1.5 \times 10^{-5}} = 6 \times 10^8.$$

$$\text{drag} = C_f \frac{1}{2} \rho U^2 L p D = 0.073(6 \times 10^8)^{-1/5} \times \frac{1}{2} \times 1.2 \times 15^2 \times 600 \times p \times 100 = 32600 \text{ N}$$

$$\text{power} = F_D \times U = 32600 \times 15 = 489000 \text{ W or } 655 \text{ hp or } \underline{164 \text{ hp/engine.}}$$

$$\text{b) } \rho_{\text{helium}} = \frac{p}{RT} = \frac{100}{2.077 \times 288} = 0.167 \text{ kg/m}^3.$$

$$F_B = W_{\text{air}} - W_{\text{helium}} = \Delta \rho \times V = (1.2 - 0.167) \times 9.8 \times p \times 50^2 \times 600 / 2 = 2.38 \times 10^7$$

$$\text{payload} = F_B - W = 23.8 \times 10^6 - 9.8 \times 1.2 \times 10^6 = \underline{12 \times 10^6 \text{ N}}$$

$$8.124 \quad u = \frac{f_y}{f_x}, \quad \frac{f_u}{f_x} = \frac{f^2_y}{f_x f_y}, \quad v = -\frac{f_y}{f_x}, \quad \frac{f_u}{f_y} = \frac{f^2_y}{f_y^2}, \quad \frac{f^2_u}{f_y^2} = \frac{f^3_y}{f_y^3}.$$

Substitute into Eq. 8.6.45 (with $dp/dx = 0$):

$$\frac{f_y}{f_x} \frac{f^2_y}{f_x f_y} - \frac{f_y}{f_x} \frac{f^2_y}{f_y^2} = n \frac{f^3_y}{f_y^3}.$$

8.125 We also have

$$\frac{f_y}{f_x} = \frac{f_y}{f_x} \frac{f_f}{f_x} + \frac{f_y}{f_h} \frac{f_h}{f_x}, \quad \frac{f^2_y}{f_x f_y} = \frac{f(f_y/f_x) f_f}{f_x} + \frac{f(f_y/f_x) f_h}{f_h f_x}$$

Recognizing that $f_f/f_x = 1$, $f_f/f_y = 0$, $f_h/f_x = -\frac{y}{2} \sqrt{U_\infty/nx^3}$, and

$$\frac{f_h}{f_y} = \sqrt{U_\infty/nx}, \quad \frac{f_y}{f_x} = \sqrt{\frac{U_\infty}{nf}} \frac{f_y}{f_h}, \quad \frac{f_y}{f_x} = \frac{f_y}{f_f} - \frac{y}{2} \sqrt{\frac{U_\infty}{nx^3}} \frac{f_y}{f_h}$$

$$\frac{f^2_y}{f_x f_y} = \sqrt{\frac{U_\infty}{nf}} \frac{f^2_y}{f_f f_h} - \frac{1}{2} \sqrt{\frac{U_\infty}{nf^3}} \frac{f_y}{f_h} + \sqrt{\frac{U_\infty}{nf}} \frac{f^2_y}{f_h^2} \left(-\frac{y}{2} \sqrt{\frac{U_\infty}{nf^3}} \right)$$

$$\frac{f^2_y}{f_y^2} = \sqrt{\frac{U_\infty}{nf}} \frac{f^2_y}{f_h^2} \left(\sqrt{\frac{U_\infty}{nf}} \right), \quad \frac{f^3_y}{f_y^3} = \frac{U_\infty}{nf} \frac{f^3_y}{f_h^3} \sqrt{\frac{U_\infty}{nf}}$$

Equation 8.6.47 then becomes, using $\sqrt{U_\infty/nf} = h/y$,

$$\frac{h}{y} \frac{f_y}{f_h} \left(\frac{h}{y} \frac{f^2_y}{f_f f_h} - \frac{h}{2yx} \frac{f_y}{f_h} - \frac{h^2}{2yx} \frac{f^2_y}{f_h^2} \right) - \left(\frac{f_y}{f_f} - \frac{h}{2x} \frac{f_y}{f_h} \right) \left(\frac{h^2}{y^2} \right) \frac{f^2_y}{f_h^2}$$

$$= n \frac{U_\infty}{nx} \frac{h}{y} \frac{f^3_y}{f_h^3}$$

Multiply by y^2/h^2 and Eq. 8.6.49 results:

$$-\frac{1}{2f} \left(\frac{f_y}{f_h} \right)^2 + \frac{f^2_y}{f_f f_h} \frac{f_y}{f_h} - \frac{f_y}{f_f} \frac{f^2_y}{f_h^2} = n \frac{f^3_y}{f_h^3} \sqrt{\frac{U_\infty}{nf}}$$

$$8.126 \quad u = \frac{f_y}{f_y} = \sqrt{U_\infty n x} \frac{dF}{dh} \frac{f_h}{f_y} = \sqrt{U_\infty n x} F(h) \sqrt{\frac{U_\infty}{n x}} = \underline{U_\infty F(h)}.$$

We used Eq. 8.6.50 and Eqs. 8.6.48.

$$\begin{aligned} v &= -\frac{f_y}{f_x} = -\frac{f}{f_x} (\sqrt{U_\infty n x} F) = -\frac{1}{2} \sqrt{\frac{U_\infty n}{x}} F - \sqrt{U_\infty n x} \frac{fF}{f_h f_x} \\ &= -\frac{1}{2} \sqrt{\frac{U_\infty n}{x}} F - \sqrt{U_\infty n x} F y \sqrt{\frac{U_\infty}{n}} \left(-\frac{1}{2} x^{-3/2} \right) \\ &= -\frac{1}{2} \sqrt{\frac{U_\infty n}{x}} F + \frac{y}{2} \sqrt{\frac{U_\infty}{n x}} \sqrt{\frac{U_\infty n}{x}} F = \underline{\frac{1}{2} \sqrt{\frac{U_\infty n}{x}} (hF - F)}. \end{aligned}$$

8.127 The results are shown in Table 8.5.

$$8.128 \quad \text{a) } t_0 = 0.332 \times 1.22 \times 5^2 \sqrt{\frac{1.5 \times 10^{-5}}{2 \times 5}} = \underline{0.0124 \text{ Pa.}}$$

$$\text{b) } d = 5 \sqrt{\frac{1.5 \times 10^{-5} \times 2}{5}} = \underline{0.0122 \text{ m.}}$$

$$\text{c) } v_{\max} = \sqrt{\frac{n U_\infty}{x}} \left[\frac{1}{2} (hF - F) \right]_{\max} = \sqrt{\frac{1.5 \times 10^{-5} \times 5}{2}} \times 0.8605 = \underline{0.00527 \text{ m/s.}}$$

$$\begin{aligned} \text{d) } Q &= \int_0^d u dy = \int_0^d U_\infty \frac{dF}{dh} dy = \int_0^d U_\infty \frac{dF}{dh} dh \sqrt{\frac{v x}{U_\infty}} \\ &= U_\infty \sqrt{\frac{n x}{U_\infty}} [F(d) - F(0)] = 5 \sqrt{\frac{1.5 \times 10^{-5} \times 2}{5}} \times 3.28 = \underline{0.04 \text{ m}^2 / \text{s} / \text{m}} \end{aligned}$$

$$8.129 \quad \text{a) } t_0 = 0.332 \times 0.0024 \times 15^2 \sqrt{\frac{1.6 \times 10^{-4}}{6 \times 15}} = \underline{2.39 \times 10^{-4} \text{ psf.}}$$

$$\text{b) } d = 5 \sqrt{\frac{1.6 \times 10^{-4} \times 6}{15}} = \underline{0.04 \text{ ft.}}$$

$$\text{c) } v_{\max} = \sqrt{\frac{n U_\infty}{x}} \left[\frac{1}{2} (hF - F) \right]_{\max} = \sqrt{\frac{1.6 \times 10^{-4} \times 15}{6}} \times 0.8605 = \underline{0.0172 \text{ fps.}}$$

$$\text{d) } Q = \int_0^d u dy = U_\infty \sqrt{\frac{n x}{U_\infty}} F(d) = 15 \sqrt{\frac{1.6 \times 10^{-4} \times 6}{15}} \times 3.28 = \underline{0.394 \text{ ft}^2 / \text{sec} / \text{ft.}}$$

8.130 At $x = 2\text{m}$, $\text{Re} = 5 \times 2 / 10^{-6} = 10^7$. \therefore Assume turbulent from the leading edge.

$$\text{a) } t_0 = \frac{1}{2} r U_\infty^2 \frac{0.455}{(\ln 0.06 \text{Re}_x)^2}$$

$$= \frac{1}{2} \times 1000 \times 5^2 \frac{0.455}{(\ln 0.06 \times 10^7)^2} = \underline{32.1 \text{ Pa}}$$

b) $u_t = \sqrt{t_0 / r} = \sqrt{32.1 / 1000} = 0.1792 \text{ m / s}$

$$\frac{5}{0.1792} = 2.44 \ln \frac{0.1792d}{10^{-6}} + 7.4. \quad \therefore d = 0.0248 \text{ m or } \underline{24.8 \text{ mm}}$$

c) Use the 1/7 the power-law equation:

$$Q = \int_0^{0.0248} 5(y / 0.0248)^{1/7} dy = \underline{0.109 \text{ m}^3 / \text{s} / \text{m}}$$

8.131 From Table 8.5 we would select $h = 6$:

a) $d = 6 \sqrt{\frac{nx}{U_\infty}} = 6 \sqrt{\frac{1.5 \times 10^{-5} \times 2}{5}} = \underline{0.0147 \text{ m}}$

b) $d = 6 \sqrt{\frac{nx}{U_\infty}} = 6 \sqrt{\frac{15.8 \times 10^{-5} \times 6}{15}} = \underline{0.047 \text{ ft or } 0.57 \text{ in.}}$

8.132 From Table 8.5 we interpolate for $F = 0.5$ to be

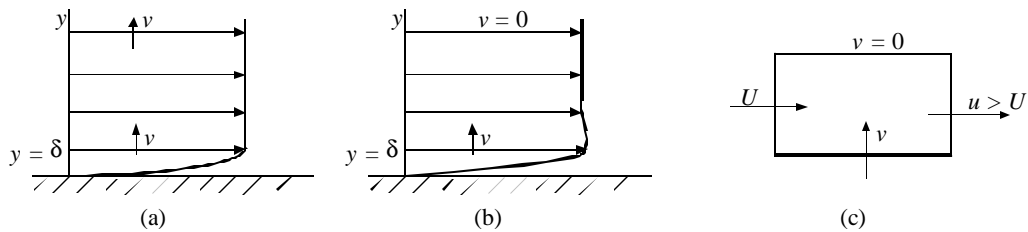
$$h = \frac{0.5 - 0.3298}{0.6298 - 0.3298} (2 - 1) + 1 = 1.57$$

$$= y \sqrt{\frac{5}{1.5 \times 10^{-5} \times 2}}. \quad \therefore y = 0.00385 \text{ m or } \underline{3.85 \text{ mm}}$$

$$v = \sqrt{\frac{nU_\infty}{x}} \left(\frac{1}{2} \right) (hF - F) = \sqrt{\frac{1.5 \times 10^{-5} \times 5}{2}} (0.207) = \underline{0.00127 \text{ m / s}}$$

$$t = m \left(\frac{\int u}{\int y} + \frac{\int y}{\int x} \right) = F'' r U_\infty^2 \sqrt{\frac{n}{x U_\infty}} = 0.291 (1.2) 5^2 \sqrt{\frac{1.5 \times 10^{-5}}{2 \times 5}} = \underline{0.011 \text{ Pa}}$$

8.133

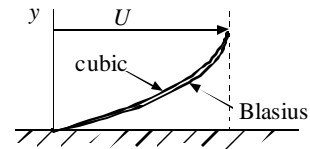


If $v = 0$ at $y = 10d$ and $v > 0$ at $y = d$, then $\int u / \int y < 0$ and continuity demands that $\int u / \int x > 0$. The u component, for $y > d$ must then be greater than U , as shown in (b); there should be a slight “overshoot”. Also, consider the control volume of (c) where the lower boundary is just above $y = d$. If $v = 0$ at large y , say $y = 10d$, then continuity demands that u out the right area be greater than U : an “overshoot”. It is not reasonable to assume that $v = \text{const}$ as in (a);

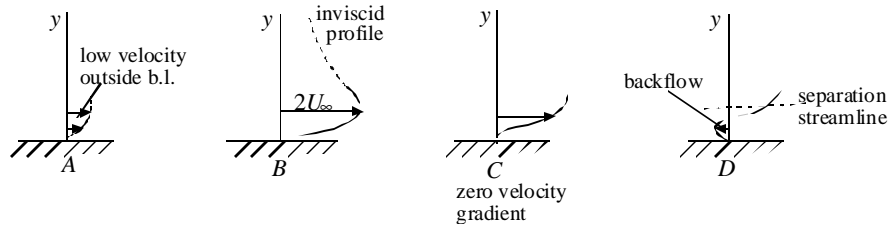
reality would demand a profile such as that sketched in (b). The overshoot would be quite small and is neglected in boundary layer theory.

8.134
$$u = U_{\infty} \left(\frac{3y}{2d} - \frac{1}{2} \frac{y^3}{d^3} \right)$$

For the Blasius profile: see Table 8.5.
 (This is only a sketch. The student is encouraged to draw the profiles to scale.)



8.135



- 8.136 A: $\frac{\partial p}{\partial x} < 0$. (favorable)
 B: $\frac{\partial p}{\partial x} \cong 0$.
 C: $\frac{\partial p}{\partial x} > 0$. (unfavorable)
 D: $\frac{\partial p}{\partial x} > 0$.
 E: $\frac{\partial p}{\partial x} < 0$.

